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(54) Title: CLEANING OF HYDROCARBON-CONTAINING MATERIALS WITH CRITICAL AND SUPERCRITICAL SOLVENTS

(57) Abstract: A method for cleaning materials containing solids and/or liquids is disclosed which involves contacting the materials with an extracting fluid including Xe, NH₃, lower aromatics, nitrous oxide, water, CO, CO₂, H₂O, lower alcohols, lower alkanes, lower alkenes, or mixtures or combinations thereof under conditions of temperature and pressure sufficient to maintain the fluid at, near or above its critical point and to products derived therefrom.

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PATENT SPECIFICATION

TITLE: CLEANING OF HYDROCARBON-CONTAINING MATERIALS WITH CRITICAL AND SUPERCRITICAL SOLVENTS

RELATED APPLICATION

This application is a Continuation-in-Part of United States Patent Application Serial No.

10/066,291 filed 31 January 2002, which claims provisional priority to United States Provisional Application Serial No. 60/265,825 filed 1 February 2000.

BACKGROUND OF THE INVENTION

1. Field of the Invention

[0001] The present invention relates to an efficient and cost effective method for treating hydrocarbon-containing materials to remove solids, water, sulfur and/or other contaminants.

[0002] More particularly, the present invention relates to a method for cleaning hydrocarbon-containing materials including oil-containing materials such as well-fluids, drilling fluids, used oils, oil contaminated soils, or the like, under near critical, critical and/or supercritical conditions to produce a clean solid residue, an hydrocarbon residue and an aqueous residue, where the hydrocarbon residue is reusable, the solid residue is substantially free of hydrocarbons and aqueously extractable contaminants and the aqueous residue can be further cleaned to produce a purified water residue.

2. Description of the Related Art

[0003] Critical and supercritical extraction processes have been known for some time. Supercritical extraction has been used to clean oil and to desulfurize coal, but the technique has not been used to clean up drilling fluids so that the cutting are substantially free of hydrocarbon residue and/or aqueously soluble contaminants.

[0004] Thus, there is a need in the art for a method for cleaning drilling fluids and solid concentration derived therefrom generally via centrifugation to a purified solid material substantially free of hydrocarbon residues, drilling field chemicals and/or water soluble contaminants.

SUMMARY OF THE INVENTION

[0005] The present invention provides a solid residue substantially free of organic and/or non-organic water-soluble components, where the solid residue is derived from critical and/or supercritical extraction of a material including the solid, organic and/or non-organic water-

soluble components with a cleaning composition comprising CO, CO₂, H₂O, lower alcohols, lower alkanes, lower alkenes or mixtures or combinations thereof.

[0006] The present invention provides a slurry residue substantially free of organic components, where the slurry residue is derived from near critical, critical and/or supercritical extraction of a material including the solid, organic and/or non-organic water-soluble components and water with a cleaning composition comprising CO, CO₂, H₂O, lower alcohols, lower alkanes, lower alkenes or mixtures or combinations thereof.

[0007] The present invention provides a water-insoluble liquid residue substantially free of solids and/or non-organic water-soluble components, where the liquid residue is derived from critical and/or supercritical extraction of a material including the solid, organic and/or non-organic water-soluble components with a cleaning composition comprising CO, CO₂, H₂O, lower alcohols, lower alkanes, lower alkenes or mixtures or combinations thereof.

[0008] The present invention provides a hydrocarbon residue substantially free of solids and/or water soluble components including organic and inorganic, water-soluble components or mixtures thereof, where the hydrocarbon liquid residue is derived from critical and/or supercritical extraction of a material including the solid, organic and/or non-organic water-soluble components with a cleaning composition comprising CO, CO₂, H₂O, lower alcohols, lower alkanes, lower alkenes or mixtures or combinations thereof.

[0009] The present invention provides a method for cleaning a solid material including contacting the mixture with a cleaning composition including CO, CO₂, H₂O, lower alcohols, lower alkanes, lower alkenes or mixtures or combinations thereof under conditions of temperature and pressure sufficient to maintain the cleaning composition at, near or above its critical point for a time sufficient to achieve a desired degree of cleaning of the solid material.

[0010] The present invention provides a method for cleaning a solid material including contacting the mixture with a cleaning composition including CO, CO₂, H₂O, lower alcohols, lower alkanes, lower alkenes or mixtures or combinations thereof under conditions of temperature and pressure sufficient to maintain the cleaning composition at, near or above its critical point for a time sufficient to achieve a desired degree of cleaning of the solid material to form an organic residue and a mixture of water and the solid material, which can be in the form of an aqueous slurry, dispersion, suspension or other aqueous/solid mixture.

[0011] The present invention provides a method for cleaning a mixture including contacting the mixture with a cleaning composition including CO, CO₂, H₂O, lower alcohols, lower

alkanes, lower alkenes or mixtures or combinations thereof under conditions of temperature and pressure sufficient to maintain the cleaning composition at, near or above its critical point for a time sufficient to achieve a desired degree of separation of the mixture.

[0012] The present invention provides a method for cleaning a mixture including contacting the mixture including a solid component, a water-insoluble liquid component and water with a cleaning composition including CO, CO₂, H₂O, lower alcohols, lower alkanes, lower alkenes or mixtures or combinations thereof under conditions of temperature and pressure sufficient to maintain the cleaning composition at, near or above its critical point for a time sufficient to achieve a desired degree of separation of the mixture into a solid residue, a water-insoluble liquid residue and an water-soluble liquid residue.

[0013] The present invention provides a method for cleaning a mixture including contacting the mixture including a solid component, a water-insoluble liquid component and water with a cleaning composition including CO, CO₂, H₂O, lower alcohols, lower alkanes, lower alkenes or mixtures or combinations thereof under conditions of temperature and pressure sufficient to maintain the cleaning composition at, near or above its critical point for a time sufficient to achieve a desired degree of separation of the mixture into a solid residue, a water-insoluble liquid residue and/or an water-soluble liquid residue, where the solid residue is substantially free of organic and aqueously soluble components, the water-insoluble liquid residue is substantially free of solids, water or water-soluble components, and the water-soluble liquid residue is substantially free of solids and water-insoluble liquid components.

[0014] The present invention provides a method for cleaning a mixture containing solids, organics such as hydrocarbons, inorganics such as metal complexes, and/or water including contacting the mixture with a cleaning composition including CO, CO₂, H₂O, lower alcohols, lower alkanes, lower alkenes or mixtures or combinations thereof under conditions of temperature and pressure sufficient to maintain the composition in a supercritical state for a time sufficient to achieve a desired degree of component separation.

[0015] The present invention provides a method for cleaning drilling fluids, oil contaminated soil, oil pit material, or the like including contacting a drilling fluid with a cleaning composition including CO, CO₂, H₂O, lower alcohols, lower alkanes, lower alkenes or mixtures or combinations thereof under near critical, critical or supercritical conditions.

[0016] The present invention provides a method for cleaning used motor oils including contacting a used-motor oil with a cleaning composition including CO, CO₂, H₂O, lower

alcohols, lower alkanes, lower alkenes or mixtures or combinations thereof under near critical, critical or supercritical conditions, to produce a reusable motor oil. Preferably, the reusable motor oil is substantially clear in color and has the characteristic of the motor oil prior to the addition of one or more additives, especially polar and/or water soluble additives. The reusable motor oil also generally has a lower sulfur content than the sulfur content found in the used motor oil prior to cleaning.

[0017] The present invention provides a method for desulfurizing a hydrocarbon fuel such as fuel oil, gasoline, diesel fuel, jet fuel or similar hydrocarbon fuels including contacting a hydrocarbon fuel with a composition including CO, CO₂, H₂O, lower alcohols, lower alkanes, lower alkenes or mixtures or combinations thereof under near critical, critical or supercritical conditions, to produce a hydrocarbon fuel having a sulfur content less than the sulfur content of the hydrocarbon fuel prior to cleaning.

DESCRIPTION OF THE DRAWINGS

[0018] The invention can be better understood with reference to the following detailed description together with the appended illustrative drawings in which like elements are numbered the same:

[0019] Figure 1 depicts a schematic diagram of a preferred embodiment of a batch type apparatus for carrying out the process of this invention;

[0020] Figure 2 depicts a phase diagram for carbon dioxide;

[0021] Figure 3 depicts a graph depicting the pressure verses enthalpy relationship for carbon dioxide;

[0022] Figure 4 depicts a schematic diagram of a preferred embodiment of a semi-batch apparatus for carrying out the process of this invention;

[0023] Figure 5 depicts a schematic diagram of one preferred embodiment of a continuous apparatus for carrying out the process of this invention;

[0024] Figure 6 depicts a schematic diagram of another preferred embodiment of a continuous apparatus for carrying out the process of this invention;

[0025] Figures 7A&B depict a schematic diagram of two preferred embodiment of a continuous apparatus for cleaning contaminated solid including drilling fluids, oil containing soils, or the like of this invention, where the extraction unit is shown in cross-section;

[0026] Figures 8A&B depict a schematic diagram of two preferred embodiment of a continuous multi-staged apparatus of this invention for cleaning and/or desulfurizing used

hydrocarbons including used motor oils or cleaning and/or desulfurizing hydrocarbon fuels including gasoline, fuel oil, diesel fuel, jet fuel or the like;

[0027] Figures 9A depict a schematic diagram of a preferred embodiment of a continuous multi-staged apparatus of this invention for cleaning a composition including a solid material, water, and a hydrocarbons or substantially water insoluble organics to form a hydrocarbon or organic residue substantially free of solids and/or water, a water residue substantially free of solid material and hydrocarbon, and a solid residue substantially free of water and hydrocarbon; and

[0028] Figures 9B depict a schematic diagram of a preferred embodiment of a continuous multi-staged apparatus of this invention for cleaning a composition including a solid material, water, and a hydrocarbons or substantially water insoluble organics to form a hydrocarbon or organic residue substantially free of solids and/or water and a mixture of water and the solid material.

DETAILED DESCRIPTION OF THE INVENTION

[0029] The inventors have found that an efficient and cost effective process for cleaning solid materials and/or mixtures containing solid materials can be developed using a cleaning composition at, near or above its critical point. The processes of this invention can produce a solid residue substantially free of hydrocarbons, water soluble contaminants and/or other contaminants, a water-insoluble liquid residue substantially free of solids, water-soluble contaminants and/or other contaminants and an aqueous residue substantially free of solids and water-insoluble liquid contaminants.

[0030] The present invention broadly relates to a process for cleaning solids, dispersions, slurries, and/or liquids under near critical, critical or supercritical fluid extraction where the extracting fluid includes Xe, NH₃, lower aromatics including benzene and toluene, nitrous oxide, water, CO, CO₂, H₂O, lower alcohols including methanol, ethanol, propanol, and isopropanol, lower alkanes including methane, ethane, propane, butane, pentane and hexane, petroleum ether, lower alkenes including ethylene and propylene or mixtures or combinations thereof.

[0031] The process is ideally suited for cleaning drilling fluids, reactor sludge, oil-contaminated soils, oil contaminated water, used oil, hydrocarbon fuels such as diesel fuel, jet fuel and other similar hydrocarbon fuels, extracting oils from tar sands or the like, tanker

bottoms, refinery bottoms, pit residues, refinery waste streams, refinery residue streams or the like. The pit residue include any material that comprises oil and solid materials such as soil, dirt or the like. The pit residue is generally associated with refining and/or separation and/or processing of crude oil streams. The present invention can also be used to extract hydrocarbon material out of paint wastes, polymer waste or any other chemical processing waste or waste stream that contains hydrocarbon materials, solid materials, water and/or other components that are amenable to near critical, critical and/or supercritical extraction.

[0032] The process results in purified hydrocarbons, purified solids, and/or purified water. However, near critical, critical and/or supercritical extraction is generally combined with other downstream water purification process to produce a purified water.

[0033] Drilling fluids are complex compositions that are the by-product of oil well drilling operations. These fluids can include solids from drilling operations, muds or other additives or compounds used in drilling operations, greases, anti-seize compounds, hydrocarbons from hydrocarbon bearing formations, water, heavy metals, fracturing compositions, proppants, or other ingredients and mixtures and combination thereof. Drilling fluids can be in the form of a mixture of liquids and solids, a dispersions, a suspension, an emulsion, or any other liquid like mixture of solids and liquids.

[0034] Drilling fluid solids are solids obtained from an initial separation of solids from liquid components of a drilling fluid mixture. The solids are generally obtained via centrifugation of the drilling fluids as is well-known in the art. The solids generally have the appearance of a tar like material, but can be any solid like material derived from a process which removes most liquid material from the drilling fluids.

[0035] The process is also ideally suited for cleaning hydrocarbon-containing fuels such as diesel fuel, jet fuel, home heating oil and other similar hydrocarbon fuels, or even gasoline. The process results in purified hydrocarbon-containing fuels having reduced sulfur contents and a sulfur containing residue. The fuel to be treated is contacted with a treating solvent or composition under near critical, critical and/or supercritical conditions of temperature and pressure. The treatment temperature is usually from about 100° to about 400°C.

[0036] The process is also ideally suited for cleaning used motor oils to produce a reusable motor oil. Because the cleaning process removes material that are polar, many to all of the polar additives may be removed during the extraction system. Therefore, in one preferred reusable oil product of this invention, additives or additive packages are added into the

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cleaned oil. These additives can include any additive currently added to motor oils to improve their detergent properties or other properties.

[0037] Suitable extracting fluid include, without limitation, Xe, NH₃, lower aromatic such as benzene, toluene, or xylene, nitrous oxide, water, CO, CO₂, H₂O, lower alcohols such as methanol, ethanol, propanol, or isopropanol, lower alkanes such as methane, ethane, propane, butane, pentane hexane, or petroleum ether; lower alkenes such as ethylene or propylene; or mixtures or combinations thereof. Preferably, the extracting fluid includes carbon dioxide, water, lower alkanes, lower alcohols, or mixture or combinations thereof. Particularly, the extracting fluid comprises a major portion of CO₂ and a minor portion of a secondary fluid selected from the groups consisting of Xe, NH₃, lower aromatics, nitrous oxide, water, CO, H₂O, lower alcohols, lower alkanes, lower alkenes and mixtures or combinations thereof, where a major portion means greater than 50 mol% carbon dioxide, preferably, greater than 70 mol% carbon dioxide, particularly, greater than 90 mol% carbon dioxide, and especially, greater than 95 mol% carbon dioxide. More particularly, the extracting fluid is exclusively carbon dioxide.

[0038] Tabulated below are critical conditions for various supercritical fluids:

Fluid	Critical temperature T _c (°K)	Critical pressure P _c (MPa)	Critical Volume V _c (cm ³ /mol)
Carbon dioxide	304.14	7.375	94
Water	647.14	22.06	56
Ethane	305.32	4.872	145.5
Ethene	282.34	5.041	131
Propane	369.83	4.248	200
Xenon	289.73	5.84	118
Ammonia	405.5	11.35	75
Nitrous oxide	309.57	7.255	97
Fluoroform	299.3	4.858	133
Methanol	190.56	4.599	98.60
Isopropanol	508.3	4.764	222
Toluene	591.75	4.108	316

[0039] For the purposes of this invention, the term substantially free means that the cleaned component includes less than or equal to about 5 wt% of any given contaminant, preferably, less than or equal to about 2.5 wt% of any given contaminant, particularly less than or equal to about 2 wt% of any given contaminant and especially less than or equal 1 wt% of any contaminant.

[0040] The material-to-be-treated is contacted with treating solvent under supercritical conditions of temperature and pressure. The term, "supercritical," "supercritical state," "supercritical conditions," or "supercritical conditions of temperature and pressure," refers to a temperature above the critical temperature (T_c) of the solvent being used, and a pressure above the critical pressure (P_c) of the solvent being used. The treatment temperature is usually from 470° to 630°K. All temperatures herein will be given in degrees Kelvin (°K) or degree Celsius (°C) unless otherwise stated. Treatment according to this invention is carried out at a reduced temperature (T_r) from 1.0 to about 1.4, preferably from about 1.05 to about 1.3, and at a reduced pressure (p_r) from 1.0 to about 2.0, preferably from about 1.05 to about 1.5. The term, "critical," "critical state," "critical conditions" or "critical conditions of temperature and pressure," refers to a solvent at its critical temperature, T_c , and its critical pressure, P_c . The term, "near critical," "near critical state," "near critical conditions" or "near critical conditions of temperature and pressure," refers to a solvent at most about 10°C below its critical temperature, T_c , and at most about 10 psi below its critical pressure, P_c , and preferably, at most about 5°C below its critical temperature, T_c , and at most about 5 psi below its critical pressure, P_c .

[0041] The solvent to material-to-be-treated ratio for treatment according to this invention can range from about 0.2 to about 3 kilograms of solvent per kilogram of material-to-be-treated (Kg/Kg) preferably from about 0.3 to about 1.0 Kg/Kg. Actually, the solvent to material-to-be-treated ratio is a dimensionless number, since both the amount of solvent and the amount of material-to-be-treated are expressed on a weight basis.

[0042] The present invention can make possible the use of a much lower solvent to material-to-be-treated ratio than those used in prior art processes at the lower end of the solvent to material-to-be-treated range. However, the process of the present invention can be operated at any ratio to achieve a desired result.

[0043] The solvent flow rate is generally from about 0.2 to 3 kilograms per hour of solvent per kilogram of material-to-be-treated per hour (*i.e.*, 0.2 to 3 kg/kg-hr). Preferably the solvent

flow rate is about 0.5 kg/kg-hr. The time of treatment may range from about 0.5 to about two hours, and is preferably about one hour.

[0044] The material-to-be-treated may be treated in either a single stage or in plurality of stages (*i.e.*, in two or more stages). In single stage extractions or treatments, the composition of the treating solvent remains uniform over the entire course of treatment, and can be any solvent described above, but is preferably carbon dioxide alone or in combination with water, a lower alcohol or a lower hydrocarbon. In plural stage extractions or treatments, the composition of the treating solvent can be the same or different from stage to stage. For some using multi-staged treatment applications, the critical temperature of the treating solvent used in each stage increases progressively. Thus, the first stage solvent may be a carbon dioxide; next a mixture of carbon dioxide and water, or carbon dioxide and methanol; the solvent for the next stage may be, for example, a mixture of methanol and water with no carbon dioxide and so on. In extreme cases, the material-to-be-treated may be contacted consecutively with each of the treating fluids, *i.e.*, first with carbon dioxide, then with methanol, and finally with water, each in pure or substantially pure form. Whenever the composition of the solvent is varied over the course of treatment, the overall solvent composition (based on the total quantities of each treating fluid used over the entire course of treatment) is as stated above, *i.e.*, the mole fraction of carbon dioxide is from 0 to 0.5 (preferably 0.05 to 0.25), the mole fraction of methanol is from 0.20 to 0.70 (preferably 0.30 to 0.50), and the mole fraction of water is from 0.20 to 0.70 (preferably 0.25 to 0.65).

[0045] In many of the preferred processes of this invention, carbon dioxide alone is the preferred extraction fluid. Thus, in multistage application, only the amount of carbon dioxide being supplied to each stage may vary. Again, the carbon dioxide supplied in the first stage progresses with the material-to-be-treated to the next stage. Thus as additional carbon dioxide is supplied, the ratio to carbon dioxide to the material-to-be-treated changes. Additionally, each stage can be operated at a different temperature and/or pressure to achieve a desired final product.

[0046] For solid type materials, a fixed bed, a moving bed reactor or other similar reactors can be used. Such reactor systems are described in more detail hereinafter. When the material-to-be-treated is a fluid (slurry, liquid, dispersion, suspension, mixture, or the like) at treatment temperature, a conventional stirred reactor or other type of batch, semi-batch or continuous reaction system can be used. For materials that include a large amount of solids

such as drilling fluids, a preferred continuous system includes a tube within a tube within a tube type reactor described in more detail in disclosure associated with Figure 8. For materials, such as used motor oil, which generally, do not include a large amount of solids, a preferred system includes a series of extraction units described in more detail in the disclosure associated with Figure 9. This same type of multi-staged systems is ideally suited for reducing the sulfur content of hydrocarbon based fuels.

[0047] This invention will be further described and illustrated with reference to the drawings which represent preferred embodiments of systems for carrying out the processes of this invention, *i.e.*, processes designed to convert drilling fluids and solids therefrom into a cleaned solid residue, a non-aqueous residue and an aqueous residue.

System and System Operation

[0048] Referring now to Figure 1, a preferred embodiment of an extraction system generally 100 for use in the present invention is shown to include a source of a supercritical solvent 102, in this case carbon dioxide. The source 102 is connected to a sight glass 104 and a filter 106 via tubing 108. The tubing 108 is also connected to a rupture disk relief valve 110 for safety purposes. The filter 104 is connected to a pump 112 having a back pressure regulator 114 via tubing 108. The pump 112 is connected to a top entry 116 of an extraction cell 118 via tubing 108 including a pressure gauge 120, a supply control valve 122 and a second rupture disk relief valve 124. The cell 118 includes a bottom entry 126 and a sensor 128. The top entry 116 is also connected to a top outlet valve 130 via tubing 108; the bottom entry 126 is connected to a bottom outlet valve 132 and a bleed control valve 134, which is internally connected to a bleed valve 136. The top and bottom outlet control valves 130 and 132 are connected to a separation vessel 138 via a separator control 140 and a heat exchanger 142 including a second pressure gauge 144 and a bleed valve 146. The separator 138 includes a sensor 148, a carbon dioxide outlet 150 and a cleaned material outlet 152 having a control valve 154 which can be connected to a cleaned material container (not shown). The carbon dioxide outlet 150 connects to a used carbon dioxide venting line 156 which includes a back pressure regulator 158, two filter 160, an flow regulator 162 and an exhaust line 164, which can be a recycle line by connecting the line to the pump 112. The entire system is amenable to computer control using standard computer control systems as are all of the other systems described herein.

[0049] The system of 100 operates by charging the cell 118 with a material-to-be-treated.

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Once the cell 118 is charged, valves 130, 132, 134, and 136 are closed and valve 122 is opened to allow carbon dioxide to be pumped into the charged cell 118 via the pump 112 until a supercritical state is reached as indicated by the sensor 128. After the extraction has been allowed to run for a specified period of time, the valve 122 is closed and the pump 112 is generally turned off. After valve 112 is closed, the valves 130 and 132 are opened allowing the contents of the cell 118 to flow through valve 140, which reduces the pressure of the transferred contents, and the heat exchanger 140 to warm the contents up after pressure reduction and into the separator 138, via an inlet 139. In the separator 138, the now gaseous carbon dioxide is taken out of separator 138 through outlet 150 via venting line 156 and associated equipment to either be exhausted to the air or recycled. The cleaned material exits the separator 138 through outlet 152 controlled by the control valve 154.

[0050] The system shown in Figure 1 is a preferred embodiment of an extraction systems, but is simply an illustrative example of a system for treating mixtures containing solids, hydrocarbons and water. Both the piping and fittings together with instrumentation can be configured in many different ways to obtain the same result.

[0051] In a batch type operation, a sample is placed into a cell. The cell is then sealed and the solvent is pumped into the cell under conditions of temperature and pressure sufficient to maintain the solvent at, near or above its critical point – near critical, critical and supercritical conditions. In a continuous operation, the solvent and the material to be separated would be continuously supplied to an extraction cell and solid-containing and liquid-containing residues would be continually removed from the cell. In either case, after contacting the solvent with the sample, the liquid phase is allowed to separate into an organic phase and an aqueous phase which can then be separated by conventional means such as decantation, stripping, distillation, or the like. The solids are either removed when the cell is opened or collected continuously for post extraction treatment.

[0052] In the examples that follow a batch extraction system as shown in Figure 1 was used. The cuttings samples were placed into the chamber and the chamber or cell was then sealed. Carbon Dioxide from a standard commercial cylinder was fed into the suction side of the pump. The pump was then switched on and the pressure of CO₂ was increased until it reached the critical point. The critical point of CO₂ is a function of temperature and pressure as is the critical point for any other solvent system. For CO₂ this dependence is shown in Figure 2. Figure 2 two is a standard phase diagram generally 200 for CO₂ is shown to include

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a vapor region 202, a liquid region 204, a solid region 206 and the critical point 208. Referring now to Figure 3, a CO₂ pressure - enthalpy diagram generally is shown. The super critical fluid, CO₂, is fed into the extractor vessel whereupon the super critical fluid diffuses through the solids and removes the oil or hydrocarbons or other supercritical CO₂ soluble components, which contaminates the solid, into solution. The contaminants may be minerals, hydrocarbon (natural or synthetic). In the case of drilling fluid, the contaminants will also include additives to stabilize the drilling well fluids, including, without limitation, Polyalphaolefins, Acetals, Isomerised Olefins, Linear Alpha Olefins, Linear Alkylbenzenes, drilling muds or mixtures or combinations thereof or the like.

[0053] From the reactor vessel the solute loaded super critical fluid passes through a heated metering valve where it is depressurized and separation occurs, depositing the extracted oil and additives into the separation vessel. The super critical fluid (now in the gas phase) is exhausted to vent through a flow meter and totalizer. In a commercial full scale operation, the Carbon Dioxide gas or other fluid composition would be collected and fed back to the suction (low pressure) side of the pump, thereby creating a closed loop system. Samples of the extracted medium can be taken from the liquid phase to determine a desired degree of hydrocarbon removal. The chamber may require heating in certain circumstances.

[0054] The solid which was not taken into solution by the supercritical phase, remains in the reaction vessel for subsequent removal. After supercritical extration, the solid residue not only has reduced contaminants, preferably substantially no supercritically soluble contaminant, but is dry and a sterile.

[0055] Referring now to Figure 4, another preferred systems generally 400 for performing the extraction method of this invention is show where the extracting solvent is a mixture of carbon dioxide, pure water, and pure methanol. The pure water and pure methanol are contained in liquid form in feed reservoirs 402 and 404, respectively, having exit flow control valves 406 and 408, respectively. Liquid water and liquid methanol are introduced from reservoirs 402 and 404, respectively, into a liquid feed line 410. The water/methanol mixture is pumped through feed line 410 by means of a high pressure duplex reciprocating piston pump 412. This water/methanol mixture flows to a mixing tee 414.

[0056] Carbon dioxide is stored as a liquid under pressure in a pressure vessel 416, which may be a conventional gas cylinder. Carbon dioxide is withdrawn as a gas or vapor from the container 416 into a gas line 418. Carbon dioxide flow from the container 416 is controlled

by a pressure regulator 420. The feed rate of carbon dioxide through the line 418 to the extractor 422 is controlled by a mass flow controller 424 and a control valve 426. Carbon dioxide is then passed through a pulse suppressor 428 and a feed pre-heater 430 to insure smooth flow of the carbon dioxide stream to a gas compressor 432. Carbon dioxide is then compressed in the gas compressor 432 and the flow of compressed carbon dioxide is stabilized by passing it through a flow stabilizer 434. The carbon dioxide stream flows from the stabilizer 434 to the mixing tee 414.

[0057] The carbon dioxide stream is then mixed with the methanol/water mixture in the mixing tee 414. The combined mixture is then pre-heated in a feed pre-heater 436 to a temperature close to but slightly below the desired reaction temperature. The heated solvent mixture is then fed via a solvent feed line 438 to the extractor 422, which has a fixed or stationary bed 440 therein. The fixed bed 440 is designed to contain an amount of a composition to be subjected to supercritical extraction, where the composition is either drilling solids from a centrifuge or drilling fluids directly for a well site.

[0058] The extractor 422 is of a generally vertical tubular shape – a vertically disposed tubular reactor, which is surrounded by a heating jacket 442 having an electric heater 444 positioned therein. A foraminous plate 446 at a bottom 448 of the extractor or reactor 422 supports the bed 440. The extractor 422 is provided with a rupture disc 450 and a pressure gauge 452. The extractor 422 is also provided with a temperature sensor or indicator 454, which indicates the temperature in the bed 440, and a temperature controller 456, which controls the current to the electric heater 444 in response to a reaction temperature as sensed by temperature indicator 454.

[0059] During extraction, the extractor is held under conditions of temperature and pressure sufficient to maintain the solvent at, near, but below or above the solvents critical point – maintained under near critical, critical or supercritical conditions – as it passes downwardly through the bed 440. The effluent exits the reactor 422 at an outlet 458 and the effluent will include the solvent and some or all components soluble in the solvent (depending on the degree of intended cleaning or treatment) from the material-to-be-treated in the bed 440 such as organics, inorganics or the other compounds soluble in the extraction solvent under near critical, critical or supercritical conditions. The rate of removal of the exiting solvent is controlled by a control valve 460, which may be a needle valve. The normally liquid components of the effluent, *i.e.*, water, methanol, and liquids extracted by the solvent are

condensed by passage through a tubular condenser 462. The condenser 462 is cooled by any suitable means such as a dry ice-acetone bath 464. The condensed liquids may be removed periodically (*e.g.*, at the end of a run) from the condenser 462 for analysis. Uncondensed gases, typically carbon dioxide and normally gaseous hydrocarbons, are vented from the condenser 462 through a vent line 466. These gases may be analyzed as desired and the carbon dioxide recovered for recycling. Additionally, the volatile hydrocarbons can be collected for further processing. The calorific value of the vent gases in the line 464 may be recovered, *e.g.*, by combustion of the gas mixture, where the calorific value is sufficient to justify this. Of course, if the above reaction system is run using only one solvent component, then the other solvent component feed lines are simply turned off or by-passed.

[0060] According to a preferred embodiment of a process of this invention, centrifuged drilling solids and/or fluids are charged to the reactor 422 prior to the start of a run. Water, methanol and carbon dioxide are fed to the reactor 422 in desired proportions, which can run from pure carbon dioxide, pure methanol, pure water or any mixture or combination thereof. The respective feed rates are controlled by means of the valves 406 and 408 and the mass flow controller 424. The solvent feed mixture is pre-heated in pre-heater 436 to a temperature just below the critical temperature of the solvent composition. The solvent mixture is passed downwardly through the bed 440 in the reactor 422, where it is operated under conditions of temperature and pressure sufficient to maintain the solvent near its critical point, at its critical point or above its critical point – near critical condition, critical conditions or supercritical conditions – by means of external heat supplied by the electric heater 444. The effluent exiting the reactor 422 includes the solvent and all solvent soluble components with the solid being left in the bed 440 is continuously removed and is condensed as previously described. A run is allowed to proceed either for a predetermined length of time or for a length of time determined by some other parameter, such as instantaneous effluent analysis. Normally the solvent composition, *i.e.*, the relative proportions of water, methanol and carbon dioxide, will remain constant throughout a run. This mode of operation may be described as semi-batch, since the solids and/or fluids are charged to and the solids are discharged from the extractor 422 before and after a run, respectively, in accordance with batch operation principles, while the solvent mixture is fed continuously throughout a run. Of course, the reaction can be run with non-continuous solvent feed, which would be under purely batch operating principles.

[0061] Semi-batch operation as described in Figure 4 may be carried out in two or more stages, using solvents of different compositions in each stage. The solvent used in each stage may be Xe, NH₃, lower aromatic including benzene and toluene, nitrous oxide, water, CO, CO₂, H₂O, lower alcohols including methanol, ethanol, propanol, and isopropanol, lower alkanes including methane, ethane, propane, butane, pentane and hexane, petroleum ether, lower alkenes including ethylene and propylene or mixtures or combinations thereof. Using valves and flow controllers, an operator can pass a solvent of any desired composition into an appropriate extractor. When more than one stage is used, the first stage (the earliest portion of the run) typically uses the most volatile solvent (*i.e.*, the solvent having the lowest critical temperature), and the solvent or solvent mixtures used in subsequent operating stages typically have progressively higher critical temperatures. However, each stage can use the same solvent composition.

[0062] The present invention can also be operated under continuous operating conditions using reactors systems such as those illustrates in Figures 5 and 6. Referring now to Figure 5, a preferred continuous system generally 500 for performing the extraction method of this invention is shown to include a stirred high-pressure vessel 502, which serves to mix the material-to-be-treated such as drilling fluids or a solids with the solvent. The material-to-be-treated and the supercritical extraction solvent are fed to the vessel 502 via a feed line 504 and a solvent feed line 506, respectively. The solvent entering through the line 506 is a solvent selected from the group consisting of Xe, NH₃, lower aromatic including benzene and toluene, nitrous oxide, water, CO, CO₂, H₂O, lower alcohols including methanol, ethanol, propanol, and isopropanol, lower alkanes including methane, ethane, propane, butane, pentane and hexane, petroleum ether, lower alkenes including ethylene and propylene or mixtures or combinations thereof. The resulting slurry, dispersion or mixture is then pumped by a high-pressure slurry pump 508 through a feed preheater 510, which serves to heat up the mixture to a temperature just below the extraction temperature. The preheated feed is then admitted through a ball valve 512 or other similar device into a supercritical extractor 514 which is of the stirred reactor design, a mixing extruder, or other similar high shear mixing reactors. The mixture containing the extracted non-solid components is passed through a discharge valve 516 into a product cooler 518. The cooled product is next sent to a separating vessel 520 in which the gaseous product of extraction are separated from the cleaned solids and the liquid products. The gaseous product are either vented from the system 500 through valve 522 or

separated to recover carbon dioxide or to a system to recover hydrocarbons or to recover fuel equivalents thereof. The solid and liquid products are removed through a valved discharge line 524.

[0063] Referring now to Figure 6, another configuration for a continuous supercritical extraction system generally 600 for performing the extraction method of this invention is shown to include a storage hopper 602 containing a solid material-to-be-treated such as drilling solids, where a level of solids in the hopper 602 is controlled via a solid level indicator-controller 604. The solids are metered from the storage hopper 602 through a rotary air lock feeder 606 or via a screw type extruder or other similar apparatus into an extractor 608. A solvent mixture is fed into the extractor 608 through a solvent feed line 610. This solvent is selected from the group consisting of Xe, NH₃, lower aromatic including benzene and toluene, nitrous oxide, water, CO, CO₂, H₂O, lower alcohols including methanol, ethanol, propanol, and isopropanol, lower alkanes including methane, ethane, propane, butane, pentane and hexane, petroleum ether, lower alkenes including ethylene and propylene or mixtures or combinations thereof, which may be formed, pressurized and preheated to just below the critical temperature as described with reference to Figure 5. The solvent can be analyzed for compositional makeup using a gas chromatograph 612. The system shown in Figure 6 differs from that shown in Figure 5 in that the system of Figure 5 can be operated only co-currently, while the system of Figure 6 can be operated either under counter-current or co-current flow conditions. A mixture of extracted and cleaned solids discharged from the extractor 608 is cooled in a product cooler 614 before being let down through a valve 616 into a product separating vessel 618. In this vessel, the gaseous products of extraction are separated from the cleaned solids and the liquid products. The gaseous product is then vented from the system through a valve 620. The cleaned solids and liquid products are discharged through a valve 622 and separated as described above.

[0064] Referring now to Figures 7A&B, a preferred configuration for a continuous supercritical extraction system, generally 700, for performing the extraction method of this invention for solid and/or slurry materials is shown to include an input container 702 containing a solid material-to-be-extracted 703 such as drilling fluids.

[0065] The solids are metered from the container 702 through a control/metering system 704 into an extractor 706 via lines 707, where the control/metering system 704 can be a pump, a rotary air lock feeder, a screw type extruder, a valve, or other control/metering apparatus. It

the container 702 is pressurized, the controller 704 can be a remote controlled valve, but generally, the controller 704 is a pump.

[0066] The extractor 706 comprises a tube within a tube within a tube type extractor. The extractor 706 includes an outer column or tube 708a, a semi-permeable membrane 710, a lower section 712a and an upper section 712b. The upper section 712b includes a closed ended, inverted middle tube 708b and an inner tube 708c. The extractor 706 also includes a material-to-be-extracted inlet 714 connected to one of the lines 707 from the controller 704A. The inlet 714 passes through the membrane 710 delivering the material-to-be-extracted 703 into an interior 716 of the inner tube 708c from the container 702. The dashed lines with arrows indicate the direction of material flow in the extractor 706. The inner tube 708c extends upward to form a first gap 718a between a top 720 of the inner tube 708c and an inner surface 722 of the closed end 724 of the middle tube 708b. The middle tube 708b extends downward to form a second gap 718b between a top 711 of the membrane 710 and a bottom 726 of the middle tube 708b. While a third gap 718c is formed between an outer surface 728 of the closed end 724 of the middle tube 708b and an inner surface 730 of a top 732 of the column 708a. The inner surface 730 is shown here to include a tapered section 731 to improve material flow out of the extractor 706. The gaps 718a, 718b and 718c may have the same dimension or may have different dimensions and are designed to provide shear mixing of the material-to-be-extracted and the extracting fluid as the combined flow progressed through the extractor 706 along the path indicated by the dashed and arrowed lines.

[0067] The extractor 706 also includes extraction fluid inlets 734a, 734b and 734c adapted to supply an extraction fluid 736 from an extraction fluid supply system 738 to the extractor 706 via lines 735a-c. The inlet 734c supplies a first amount of extraction fluid 736 into the inner tube 708c at a position 740 near a top 715 of the inlet 714 via line 735c. The inlet 734b supplies a second amount of extraction fluid 736 via line 735b into the middle tube 708b at a position 742. The position 742 can be at any desired location along the middle tube 708b, but is preferably located near the gap 718b. The inlet 734a supplies a third amount of extraction fluid 736 via line 735a into the outer tube 708a at a position 744. Although the position 744 can be located anywhere along the column 708a, it is preferably located near the gap 718b.

[0068] The supply system 738 includes an extraction fluid storage tank 746, a compressor

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748, and a mass controller 750. The compressor 748 compresses the extraction fluid 736 to a desired pressure, which is preferably a pressure that is sufficient to maintain the extraction fluid in the extractor to be at or above the supercritical point for the particular extraction fluid being used. Looking at Figure 7A, the system 738 also includes separate valves 752a-c for controlling the first, second, and third amount of extracting fluid flowing into the extractor 706 through lines 735a-c and a fourth valve 752d controlling the amount of extraction fluid 736 supplied, via line 735d, to a venturi valve described below. Looking at Figure 7B, the system 738 includes only a single valve 752 for controlling the amount of extracting fluid flowing into the extractor 706 through lines 735a-c and into the venturi valve via line 735d. In both Figures 7A&B, the supply system 738 also includes a recycle line 754.

[0069] As the material-to-be-extracted 703 is being feed and mixed with the extraction fluid 736, any water and materials dissolved in the water migrate across the membrane 710 into the lower section 712a and exit the extractor 706 via a line 713 to an aqueous phase storage tank 756 via a control valve 758a and a heat exchanger 758b, where the control valve 758a reduces the pressure to ambient pressure.

[0070] After the material-to-be-extracted 703 has been mixed with the three portions of extraction fluid 736 in the extractor 706, the combined mixture exits the extractor 706 via exit line 760 which interconnects the extractor 706 with a first separator 762. The separator 762 allows the solids to sink to a bottom section 764a of the separator 762, while the fluids occupy a top section 764b of the separator 762. The separator 762 also includes a venturi valve 766 connected to an extraction fluid input 768 connected to the supply line 735d from the extraction supply system 738. As the extraction fluid 736 travels through the venturi valve 766, the solids 770 are pulled into the venturi valve 766 and exit the separator 762 to a solids recovery system 772 via a solids outlet 771. The solids recovery system includes a solids storage vessel 772a connected to the separator 762 via lines 772b having a pressure reducing control valve 772c and a heat exchanger 772d. The separator 762 can also include a by-pass outlet 769 for the extraction fluid supplied to the venturi valve 766 via inlet 768.

[0071] The liquids, oils and extraction fluid, from the first separator 762 are forwarded to a second separator 774 through two pressure-reducing control valves 776a&b and two heat exchangers 778a&b via lines 779. The second separator 774 includes hydrocarbon liquid exit line 780 connected to a hydrocarbon storage vessel 781 via control valve 782. The second separator 774 also includes probes 784, that determine the liquid level 785 in the separator

774, and an extraction fluid exit 786 connected to the extraction fluid recycle line 754. Additionally, the extraction fluid by-pass outlet 769 from the venturi valve 766 is directed via line 788 to a by-pass valve 789 and a regulator valve 790 and combined with the liquids from the first separator 762 at the heat exchanger 778a.

[0072] The preferred extraction fluid for use in the extraction system 700 is pure carbon dioxide, but the extraction fluid can be selected from the group consisting of Xe, NH₃, lower aromatic including benzene and toluene, nitrous oxide, water, CO, CO₂, H₂O, lower alcohols including methanol, ethanol, propanol, and isopropanol, lower alkanes including methane, ethane, propane, butane, pentane and hexane, petroleum ether, lower alkenes including ethylene and propylene or mixtures or combinations thereof, which may be formed, pressurized and preheated to just below the critical temperature as described with reference to Figure 5.

[0073] The apparatus of the present invention can be located remote from the drilling site or can be integrated into the drill complex. Thus, an off-shore drilling platform could have an extraction unit built onto the pumping system for the drilling fluids so that the solids and aqueous components could be separated on the hydrocarbon components which would include mud ingredients could be fed back into the downhole fluid stream.

[0074] Referring now to Figure 8A, a preferred configuration of a continuous supercritical extraction system generally 800 of this invention for cleaning and/or desulfurizing liquids with only minor amount of solids therein, such as used motor oils or fuels, is shown to include a material-to-be-treated supply system 802. The material-to-be-treated supply system 802 includes a material-to-be-treated reservoir 804 containing the material-to-be-treated 806, a pump 808 or any other apparatus for transferring a liquid material and a feed line 810.

[0075] The system 800 also includes an extracting fluid supply system 812. The extraction fluid supply system 812 includes an extracting fluid reservoir 814 containing an extraction fluid 815, a compressor 816, an extraction fluid feed line 818 and a recycle line 820.

[0076] The system 800 is a multi-staged extraction/cleaning system shown in Figure 8A to have four extractors 822a-d in series and a separator 824. Each extractor 822 includes a membrane 826 separating each extractor 822 into an upper section 828 and a lower section 830. The membranes 826 allow water and polar compounds to migrated from the upper section 828 of each extractor into the lower section of each extractor. The first extractor 822a is connected to the material-to-be-treated feed line 810, while the other three extractors 822b-

d include a forwarding line 832, which feeds the extractors 822b-d with the contents of the upper section 828 of the preceding extractor 822a-c, *i.e.*, the contents of the upper section 828 of the extractor 822a is the feed for the extractor 822b via forwarding line 832 and so on. Finally, the contents of the upper section 828 of the extractor 822d are forwarded to the separator 824 via a separator feed line 834. Each extractor 822 also includes an extractor feed line 836 connected to the feed line 818. Looking at Figure 8B, each feed line 836 includes a separate flow controlling valve 838, where the valves 838 allow the amount of extraction fluid 815 entering each extractor 822a-d to be separately controlled so that the amount of extraction fluid 815 being supplied to each extractor 822a-d can be different. Each extractor 822a-d also includes an aqueous phase outlet 840 connected to a waste aqueous storage system 842 via waste lines 844. The storage system 842 includes a pressure reduction valve 846 and a heat exchanger 848 to reduce the pressure to ambient pressure and allow the temperature to warm to room temperature and a waste water storage container 850. The waste water can be forwarded to a water treatment facility for further processing.

[0077] The separator 824 includes a finished product outlet 852 and an extraction fluid outlet 854. The finished product outlet 852 is connected to a finished product storage system 856 via finished product line 858. The finished product storage system 856 includes a pressure reduction valve 860 and a heat exchanger 862 to reduce the pressure to ambient pressure and allow the temperature to warm to room temperature and a finished product storage container 864. The extraction fluid outlet 854 is connected to the recycle line 820 passing through a pressure reduction valve 866 and a heat exchanger 868 to reduce the pressure to ambient pressure and allow the temperature to warm to room temperature prior to mixing with the fresh extraction fluid going into the compressor 816.

[0078] In the following detailed description of Figures 9A&B, two preferred reactor schematics are shown for a continuous process for separating oil and other organics (water insoluble compounds) from mixtures including solid, water and oil or other organics. The mixture can be any mixture derived from oil and/or gas exploration and/or productions such as fresh drilling fluids, used drilling fluid (drilling fluids including cutting and other solid materials entrained in the drilling fluid during drilling operations), waste pit materials which generally includes oils and/or other organics, water, and solid such as soil, cuttings, or other solid materials.

[0079] The reactors schematics shown below are similar to the reactor schematic of Figures

8A&B combined with Figures 7A&B. The reactor system includes an extraction fluid supply system, a material-to-be-treated supply system, a reactor system and two or three recovery systems depending on the type of material the user wishes to recover. If the user desires to recover an organic fraction (hydrocarbons and other substantially water insoluble organics), an aqueous fraction and a dry solids fraction, then the user would use the reactor system shown in Figure 9A. If the user desires to recover only an organic fraction and a mixed fraction of water, water soluble materials and solids, then the user would use the reactor system shown in Figure 9B.

[0080] As will be discussed below, the advantage of using the reactor system of Figure 9B, is that with sufficient heating of the mixed fraction as it is withdrawn from the reactor, each reactor can be run on a continuous basis, without having to have a staged four reactor system configuration with each individual reactor running in a batch mode. It should also be recognized that with sufficient heating of the reactor components associated with each fraction withdrawal system, each reactor can be run continuously. However, for convenience and operational expediency, a staged reactor system may have advantages because the staging can be adjusted so that one reactor can be taken off line without significantly affecting the through put of the system.

[0081] Although a four reactor system is shown below, the preferred number of reactors can range from 1 to about 12 or higher, with 2 to 10 being preferred, 3 to 8 being particularly preferred and 4 to 8 being especially preferred. When the reactor system is run as a group of batch reactors, the sequence of events for each reactor is staggered so that the entire process is continuous. Although the reactors can be scaled to any desired size and can have any desired properties, one preferred reactor design has the following properties or characteristics:

Property/Characteristic	Value	Property/Characteristic	Value
Max. Working Pressure	4,000 psig	Working Volume	94 gallons
Height	48 inches	Freeboard Volume	47 gallons
Diameter	24 inches	Plenum under filter Volume	11.75 gallons
Freeboard	24 inches ^a	½ inch Outlets	7
Plenum number Filter	6 inches ^a	1 inch Outlets	1
Parallel sides Max Height	78 inches	1¼ inch Outlets	1
Parallel sides Max ID	24 inches	1½ inch Outlets	1

^a measured to dish shoulder

[0082] Using these reactor and system specifications, the reactor cycle process is as follows: (1) 12 minute fill time @ 8 gpm (gallons per minute); (2) 3 minutes pressurization time; (3) 3 minute process time; and (4) 12 minute discharge time. These times give rise to a per reaction cycle time of 30 minutes. Thus, in a four reactor system, one reactor can be undergoing the process of each of the four steps so that the entire process is continuous and staged. Of course, for 2 to 10 reactors, the start times of each reactor can be staged to allow continuous processing. Although an 8 gpm fill rate and discharge rate are preferred, in practice the fill and discharge rates can be varied considerably from about 4 gpm to about 20 gpm or lower or higher, preferably from about 6 to about 16, particularly from about 6 to about 12 and more particularly from about 6 to about 10.

[0083] The reactor systems of Figures 9A&B are designed to operate at pressures between about 800 psig (subcritical) to about 4000 psig (supercritical) at a temperature between about 10°C and about 100°C, preferably between about 20°C and about 50°C, particularly, between about 20°C and about 40°C and more particularly between about 20°C and about 30°C or ambient. Although each reactor can be designed to run continuously at pressure, potential difficulties can arise due to expansive cooling and the formation of solid water or extraction fluid (e.g., dry ice formation) during discharge or removal of desired materials. These potential difficulties can be overcome in at least two principle ways: (1) provide sufficient heat to each fraction recovery system to prevent or reduce ice formation or (2) reduce the pressure to below about 800 psig prior to discharge. At pressure between about 600 psig and 800 psig, ice formation (water or carbon dioxide) is greatly reduced and smaller heat exchanger can be used to prevent ice formation.

[0084] The process by which the reactors system operates in a batch mode involves using control valves controlled by a controller attached either to a manual control console or a computer control console running scada processing systems as is well known in the art, with the computer control console being preferred with software sufficient to set, monitor, change and control reactor system parameters including the timing of opening and closing valves. At the start of each reactor cycle, the discharge valves of each reactor are closed via their controllers under computer or operator control.

[0085] First, fill valve associated with the material-to-be-treated supply system is opened via its controllers under computer or operator control, and the reactor is filled with the

appropriate amount of material-to-be-treated at a pressure below a pressure that would cause ice formation. After the material-to-be-treated has been charged, the material-to-be-treated fill valve is closed via its controllers under computer or operator control, and the fill valve associated with the extracting fluid supply system is then opened via its controllers under computer or operator control and at operating pressure. After the extracting fluid has been charged to the reactor, the extraction fluid fill valves is closed via its controllers under computer or operator control. All valves remained closed during the extraction process, where non-aqueous fluids are separated from solids and aqueous fluids. After the extraction time has elapsed, the pressure is lowered to a pressure below the critical pressure of the extracting fluid (generally at or below about 750 psig) and the fraction dispatch valves are opened via their controllers under computer or operator control in a given sequence.

[0086] Although the exact sequence is not critical, the preferred sequence of opening of the discharge valves is the non-aqueous (organics and extracting fluid) fraction first by opening and then closing its discharge valve via its controllers under computer or operator control. Next, the aqueous fraction second by opening and then closing its discharge valve via its controllers under computer or operator control, and followed by a dry, powdered solids fraction which is discharged by opening and then closing its discharge valve via its controllers under computer or operator control aided by a venturi valve in the reactor. Each reactor includes a water permeable screen member and/or membrane member in a lower section of the reactor so that the aqueous fraction goes into a lower portion of the reactor below the membrane and/or screen, the solid stay on the top of the member and the non-aqueous fraction occupies an upper portion of the reactor above the member. After the fractions have been discharged and their discharge valves opened and closed in the desired sequence via their controllers under computer or operator control, the process starts all over again. By staggering the cycle process for each reactor, the four reactors operate similar to an internal combustion engine where a sequence of pistons impart torque to the crank shaft in consecutive combustion events.

[0087] For reactor or reactor systems that do not require separation of the aqueous fraction from the solids fraction, but only require remove of all non-aqueous components of the material-to-be-treated, the water permeable member and the venturi valve and associated lines are removed, which converts the reactor from a three fraction discharge configuration to a two fraction discharge configuration. In the two fraction discharge configuration, reactor charging

proceeds exacting as above, which is the preferred manner of charging, because the material-to-be-treated is charged under relatively low pressure. Although high pressure charging of the material-to-be-treated is difficult because of the variability of the composition and its handling characteristics and the difficulty in equipment behavior for charging such material at high pressure. Of course, the pressure in each reactor can be raised or lowered during the course of the extraction process by adding or removing extracting fluid. Once charging and extraction are complete, the order of discharge is preferably the non-aqueous fraction first (organics and extracting fluid) and slurry second (water and solids). It should be obvious to an ordinary artisan that the aqueous phase will migrate to a lower portion of the reaction due to density as well the solid material.

[0088] Referring now to Figure 9A, a preferred configuration of a continuous extraction system generally 900 of this invention for cleaning solids such as drilling fluids including fluids that aid in the drilling operation and the fluids return from down hole which include solids, water and oil, is shown to include an extraction fluid supply system 902, a material-to-be-treated supply system 920, a reactors system 940, an oil recover system 958, a water recovery system 970 and a solids recovery system 980. While Figure 9B, shown another preferred continuous extraction system 900 includes the extraction fluid supply system 902, a material-to-be-treated supply system 920, a reactors system 940, an oil recover system 958, and a water-solids mixture recovery system 990. It should be recognized that although supercritical extraction is preferred, the reactor systems can be operated at sub-critical, critical and super-critical conditions. The reactor systems of Figures 9A&B also include a heat exchange system 1000 for exchanging heat between the extraction fluid compression step (exergonic or exothermic) and the discharge fraction step (energonic or endothermic).

[0089] The extraction fluid supply system 902 includes an extracting fluid supply reservoir 904 containing an extraction fluid 906, an intensifier 908 for comprising the extracting fluid to a desired pressure, a pressurized extracting fluid reservoir 910a, extraction fluid feed lines 912, low pressure extraction fluid recycle lines 914, and a low pressure recycle extracting fluid reservoir 910b. The supply system 902 also includes extracting fluid charging control valves 916a-d and associated controllers 918a-d.

[0090] The material-to-be-treated supply system 920 includes a material-to-be-treated supply reservoir 922, a pressurization system 924 for charging the material-to-be-treated via material-to-be-treated supply lines 926. The supply system 920 also includes material-to-be-

treated charging control valves 928a-d and associated controllers 930a-d.

[0091] The reactors system 940 including four reactors or extractors 942a-d in parallel. Each reactor 942 includes a membrane 944 separating each reactor 942 into an upper section 946 and a lower section 948. The membranes 944 allow water and polar compounds to migrate from the upper section 946 of each reactor 942 into the lower section 948 of each reactor 942. Each reactor 942a-d is connected to the extracting fluid supply system 902 via supply lines 912, where charging is controlled by the control valves 916a-d and associated controllers 918a-d. Each reactor 942a-d is also connected to the material-to-be-treated supply system 920 via supply lines 926, where charging is controlled by the control valves 928a-d and associated controllers 930a-d. As stated above, the control valves 916a-d and 928a-d and their associated controllers 918a-d and 930a-d are timed to open so that the material-to-be-extracted is charged first at a low pressure, followed by high pressure charging of the extracting fluid. Once charged, each reactor 942 is held at pressure for a specified period of time at ambient temperature (preferred, although higher and lower temperatures can be used with concurrent pressure adjustment) to promote complete extraction. Of course, the reactors 942 can also, and preferably do, include pressure sensors 950a-d, temperatures sensors 952a-d and level sensors 954a-d.

[0092] The oil recover system 958 includes a non-aqueous or oil fraction outlet 959 connected to a separation tank 960 via oil fraction recovery lines 961 including an oil fraction discharge valves 962a-d and their associated controllers 963a-d. The separator tank 960 allows the extraction fluid to transition to the gas phase and includes an oil outlet 964 connected to a finished product storage system 965 via finished product line 966. The tank 960 also includes an extracting fluid outlet 967 which is connected to the extraction supply system 902 via return lines 968.

[0093] The water recovery system 970 includes an aqueous fraction outlet 971 connected to an aqueous fraction storage tank 972 via aqueous fraction recovery lines 973 including aqueous fraction discharge valves 974a-d and their associated controllers 975a-d.

[0094] The solids recovery system 980 includes a solids fraction outlet 981 connected to a separation tank 982 via solids fraction recovery lines 983 including solids fraction discharge valves 984a-d and their associated controllers 985a-d and venturi valves 986a-d located inside the upper section 946 of the reactors 942. The separator tank 982 includes an extracting fluid outlet 987 connected to the recycle lines 914 and a solids outlet 988.

[0095] Referring to Figure 9B, the reactors 942 do not include the membrane 944, the aqueous recovery system 970 and the solids recovery system 980. Instead, the water recovery system 970 and the solids recovery system 980 are combined into a single water-solids mixture recovery system 990, where the system 990 includes a mixed fraction outlet 991 connected to a storage tank 992 via mixed fraction recovery lines 993 including mixed fraction discharge valves 994a-d and their associated controllers 995a-d.

[0096] In addition to the features and aspects of the reactor systems of Figures 9A&B, the reactor system also include a heat exchange system 1000. The heat exchange system 1000 is adapted to utilize the heat generated during the extraction fluid compressing step to warm the reactor systems and recovery lines during the discharge process. The heat exchange system 1000 includes a first heat exchanger 1002 associated with the intensifier 908 for withdrawing heat generated in the compression step and carrying the heat via a heat exchange fluid through heat exchange lines 1004 to reactor heat exchangers 1006 and recovery line heat exchangers 1008. Thus, heat generated in transitioning the low pressure extracting fluid (gas) to high pressure extracting fluid (liquid) is used to counteract the cooling due to the transition of the extracting fluid from its high pressure state (liquid) to its low pressure state (gas), preventing ice and/or dry ice formation in the reactor or discharge lines or valves during the discharge process.

[0097] Although any extraction fluid described in this invention can be used in the systems of Figures 7A&B, 8A&B and 9A&B, the system preferably uses pure carbon dioxide.

[0098] Additionally, if carbon dioxide is used in the extraction solvent composition, then any of the previously described installation can be equipped with a low temperature separator for separating carbon dioxide out of the atmosphere. Additionally, the apparatus can have recycling equipped to recover the extraction solvent for recycling.

EXPERIMENTAL RESULTS

[0099] The supercritical extraction solvent used in the following examples was standard commercial grade Carbon Dioxide, from a stock cylinder. The type of cell used in the following examples was an 8 mL stainless steel view cell. The pump type used in the following examples was a Milton Roy 100ml/hour max, positive displacement pump. The samples used in the following examples was a sample as received from Baker Hughes and was centrifuged cuttings from well fluids. In all of the examples the follow, the oil removal % was estimated or derived by sight only.

Example 1

[0100] This example illustrates the cleanup of a sample of oil laden solids obtained after well fluids are subjected to centrifugation under supercritical conditions using CO₂ at 3,500 psi.

[0101] The supercritical extraction cell and pipework were cleaned with acetone. 1 g of the sample was placed in the cell and the cell was reassembled. The cell was then placed into supercritical pipe circuit. The cell and pipework were flushed twice with stock Carbon Dioxide. The pressure was then increased to about 3,500 psi at ambient temperature. No color change in liquid phase was noted. The pressure was held at about 3,500 psi pressure for about 1 hour and 20 minutes. The total oil removed from the sample was about 99%. The solid material had a slight hydrocarbon sent, but dry to the touch.

Example 2

[0102] This example illustrates the cleanup of a sample of oil laden solids obtained after well fluids are subjected to centrifugation under supercritical conditions using CO₂ at 1,000 psi and at 25°C.

[0103] The cell was cleaned and prepared as described in Example 1. After preparation, the pressure was increased to about 1000 psi at a temperature of about 25°C. The pressure and temperature were maintained for about 1 hour. Under these conditions only partial oil removal was achieved with the recovery being about 60%.

Example 3

[0104] This example illustrates the cleanup of a sample of oil laden solids obtained after well fluids are subjected to centrifugation under supercritical conditions using CO₂ at 2,000 psi and at 27.8°C.

[0105] The cell was cleaned and prepared as described in Example 1. After preparation, the pressure was increased to about 2000 psi at a temperature of about 27.8°C. The pressure and temperature were maintained for about 20 minutes. Under these conditions only partial oil removal was achieved with the recovery being about 85%.

Example 4

[0106] This example illustrates the cleanup of a sample of oil laden solids obtained after well fluids are subjected to centrifugation under supercritical conditions using CO₂ at 2,500 psi and at 22.5°C.

[0107] The cell was cleaned and prepared as described in Example 1. After preparation, the pressure was increased to about 2500 psi at a temperature of about 22.5°C. The pressure and

temperature were maintained for about 10 minutes. Under these conditions only partial oil removal was achieved with the recovery being about 95%.

Example 5

[0108] This example illustrates the cleanup of a sample of oil laden solids obtained after well fluids are subjected to centrifugation under supercritical conditions using CO₂ at 3,500 psi and at 43°C.

[0109] The cell was cleaned and prepared as described in Example 1. After preparation, the pressure was increased to about 3500 psi at a temperature of about 43°C. The pressure and temperature were maintained for about 5 minutes. Under these conditions only partial oil removal was achieved with the recovery being about 95%.

Example 6

[0110] This example illustrates the cleanup of a sample of oil laden solids obtained after well fluids are subjected to centrifugation under supercritical conditions using CO₂ at 2,500 psi and at 43°C.

[0111] The cell was cleaned and prepared as described in Example 1. After preparation, the pressure was increased to about 2500 psi at a temperature of about 43°C. The pressure and temperature were maintained for about 5 minutes. Under these conditions only partial oil removal was achieved with the recovery being about 95%.

Example 7

[0112] This example illustrates the cleanup of a sample of oil laden solids obtained after well fluids are subjected to centrifugation under supercritical conditions using CO₂ at 2,500 psi and at 23°C.

[0113] The cell was cleaned and prepared as described in Example 1. After preparation, the pressure was increased to about 2500 psi at a temperature of about 23°C. The pressure and temperature were maintained for about 5 minutes. Under these conditions only partial oil removal was achieved with the recovery being about 97%.

Example 8

This example illustrates the cleanup of a sample of oil laden solids obtained after well fluids are subjected to centrifugation under supercritical conditions using CO₂ at 2,500 psi and at 23°C.

[0114] The cell was cleaned and prepared as described in Example 1. After preparation, the pressure was increased to about 2500 psi at a temperature of about 23°C. The pressure and

temperature were maintained for about 2 minutes. Under these conditions only partial oil removal was achieved with the recovery being about 80%.

Example 9

[0115] This example illustrates an analysis of a used oil after supercritical cleanup using the apparatus of this invention and CO₂ as the extracting fluid.

[0116] The following table lists the properties of the treated oil:

Test	Common Name	Test Units	Results
ASTM D 482-95	Viscosity Index	wt%	0.365
ASTM D 93	Flash Point by PMCC	°F	230+
ASTM D 1296-99	API Gravity @60°F	°API	28.8
ASTM D 4077	Water Content	vol%	6.32
ASTM D 445	Kinematic Viscosity @100°F	cSt	24.470
ASTM D 4294-98	Total Sulfur	wt%	0.327

Example 10

[0117] This example illustrates the comparison of used oil before and after supercritical cleanup using the apparatus of this invention and CO₂ as the extracting fluid.

[0118] The following table lists the properties of the oil before treatment:

Test	Common Name	Test Units	Results
ASTM D 482-95	Ash Content	wt%	0.365
ASTM D 93	Flash Point by PMCC	°F	230+
ASTM D 1296-99	API Gravity @60°F	°API	28.8
ASTM D 4077	Water Content	vol%	6.32
ASTM D 445	Kinematic Viscosity @100°F	cSt	24.470
ASTM D 4294-98	Total Sulfur	wt%	0.327

[0119] The following table lists the properties of the oil after treatment:

Test	Common Name	Test Units	Results
ASTM D 482-95	Ash Content	wt%	0.005
ASTM D 93	Flash Point by PMCC	°F	190
ASTM D 1298	API Gravity @60°F	°API	33.9
ASTM D 4052	API Gravity @60°F	°API	33.9
ASTM D 4077	Water Content	vol%	0.08
ASTM D 445	Kinematic Viscosity @100°C	cSt	2.904
ASTM D 445	Kinematic Viscosity @100°F	cSt	11.62
ASTM D 445	Kinematic Viscosity @40°F		10.71
ASTM D 2887-97a - Ext'd	Distillation, 99% Recovery	°F	924
ASTM D 1500-98	Color	ASTM	L 2.0
ASTM D 2270-93	Viscosity Index		124
ASTM D 4530-93	Carbon Residue (micro method)		<0.1
ASTM D 4294-98	Total Sulfur	wt%	0.244
ASTM 6762	Nitrogen	mg/Kg	46.0
AAS by Acid Digestion	Iron	ppm-wt	0.4
AAS by Acid Digestion	Nickel	ppm-wt	<0.1
AAS by Acid Digestion	Copper	ppm-wt	0.2

Example 11

[0120] This example illustrates the comparison of used oil before and after supercritical cleanup using the apparatus of this invention and CO₂ as the extracting fluid.

[0121] The following table lists the properties of the oil after treatment:

Test	Value	Test	Value
Viscosity Index. D-2270	85	Viscosity CST @40°F, D-445	31.38
Appearance	Clear & Bright yellow liquid	Pour Point, °F, D-97	<-10
Odor	Petroleum	Sulfur wt%, D-4294	0.2802
Viscosity SUS @210°F, D	43.0	Ash wt%, D-482	<0.001
Viscosity SUS @100°F, D-445	154.1	Color, D-1500	1.5
Gravity API @	31.8	Actual flash point, COC D-92	400°F
Flash point, S.W. 101, °F	230+	Metals	0.10

Example 12

[0122] This example illustrates the comparison of used oil before and after supercritical cleanup using the apparatus of this invention and CO₂ as the extracting fluid.

[0123] The following table lists the properties of the oil before and after treatment:

Spec	Before	After	Diff	%Diff	+/-
Ash	0.365	0.005	0.360	98.6	Decrease
Water	6.32	0.03	6.29	99.5	Decrease
Viscosity	24.47	2.904	21.566	88.1	Decrease
Flash	190	230	40	21	Increase
API Gravity	28.8	33.9	5.1	17.7	Increase
Sulfur	0.337	0.244	0.093	27.7	Decrease

Example 13

[0124] This example illustrates the comparison of used oil before and after supercritical cleanup using the apparatus of this invention and CO₂ as the extracting fluid.

[0125] The following table lists the properties of the oil before and after treatment:

Spec	Before	After	Diff	%Diff	+/-
Ash	0.4	0.02	0.38	95	Decrease
Water	6.4	0.4	6.0	93.75	Decrease
Flash	200+	200+	----	---	---
Sulfur	0.3	0.3	---	---	---

Example 14

[0126] This example illustrates the comparison of used oil before and after supercritical cleanup using the apparatus of this invention and CO₂ as the extracting fluid.

[0127] The following table lists the properties of the oil before and after treatment:

Parameter	Test Method	Detection Limit	Before	After
Gravity API@60°F	D-287	---	28.2	29.7
Flash Point, °F	S.W. 1010	-10	BFO	380
Viscosity CST @40°C	D-445	1	24.37	35.63
Pour Point, °F	D-97	-10	<-10	<-10
Sulfur, wt%	D-4294	0.0001	0.3116	0.3019
Ash, wt%	D-482	0.001	0.315	0.004
Total Halogen, PPM	D-808	1.0	617.2	10.6
PCB's, PPM	S.W. 8082	0.05	BDL	BDL
Water by distillation, Vol%	D-95	0.05	6.4	<0.05
Sediment by Extraction, wt%	D-473	0.01	0.05	<0.01
Heat of Combustion, BTU/lb	D-240	10	17,761	19,302
Heat of Combustion, BTU/gal	D-240	60	131,04 0	141,07 8
Carbon Residue Ramsbottom, wt%	D-524	0.01	---	0.06

-33-

Heavy Metals PPM	Method	Detection Limit	Before	After
Arsenic	EPA-6010	0.0012	BDL	BDL
Cadmium	EPA-6010	0.0015	0.113	0.014
Chromium	EPA-6010	0.0040	0.525	0.007
Lead	EPA-6010	0.0140	9.693	0.338
Nickel	EPA-6010	0.0055	4.021	BDL
Sodium	EPA-6010	0.0010	66.277	1.823
Vanadium	EPA-6010	0.0020	0.030	0.015
Iron	EPA-6010	0.0015	31.981	0.351

BDL- beyond detection limit; BFO- Blows flame out @200°F

Recovery, D-86	Distillation, °F	Recovery, D-86	Distillation, °F
IBP	542	70% Recovery	728
5% Recovery	602	80% Recovery	740
10% Recovery	670	90% Recovery	756
20% Recovery	690	95% Recovery	788
30% Recovery	700	End Point	796
40% Recovery	708	Recovery	98.0%
50% Recovery	714	Residue	1.5%
60% Recovery	718	Loss	0.5%

Example 15

[0128] This example illustrates the analytical data for the oil extracted from a drilling fluid under supercritical cleanup using the apparatus of this invention and CO₂ as the extracting fluid.

[0129] The following table lists the properties of the drilling fluid recovered oil:

Parameter	Test Method	Results
Gravity API@60°F	D-287	38.0
Flash Point, PMCC °F	D-93	148
Viscosity CST @100°F	D-445	2.73
Pour Point, °F	D-97	-5
Cloud Point, °F	D-2500	10
Sulfur, wt%	D-4294	0.0615
Ash, wt%	D-482	<0.001
Color	D-15	0.5
PCB's, PPM	S.W. 8082	BDL
Water by distillation, Vol%	D-95	<0.05
Sediment by Extraction, wt%	D-473	<0.01
Carbon Residue Ramsbottom, wt%	D-524	0.06
Carbon Residue Ramsbottom, wt% on 10% residue	D-524	0.20
Cetane Index	D-976	54.0
Bacteria Count, Counts/mL	---	0
Heavy Metals PPM	Method	Before
Arsenic	EPA-6010	BDL
Cadmium	EPA-6010	BDL
Chromium	EPA-6010	0.006
Lead	EPA-6010	0.254
Nickel	EPA-6010	BDL
Sodium	EPA-6010	0.572
Vanadium	EPA-6010	BDL
Iron	EPA-6010	0.039

BDL- beyond detection limit; BFO- Blows flame out @200°F; same detection limits as in Example 14

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Recovery, D-86	Distillation, °F	Recovery, D-86	Distillation, °F
IBP	354	70% Recovery	578
5% Recovery	396	80% Recovery	600
10% Recovery	408	90% Recovery	636
20% Recovery	438	95% Recovery	674
30% Recovery	460	End Point	698
40% Recovery	482		
50% Recovery	528		
60% Recovery	554		

Accelerated Stability, F 21-61	Value
Initial Color	0.5
Final Color	1.0
Pad Rating (Blotter)	1

[0130] All references cited herein are incorporated by reference. While this invention has been described fully and completely, it should be understood that, within the scope of the appended claims, the invention may be practiced otherwise than as specifically described. Although the invention has been disclosed with reference to its preferred embodiments, from reading this description those of skill in the art may appreciate changes and modification that may be made which do not depart from the scope and spirit of the invention as described above and claimed hereafter.

CLAIMS

We claim:

1. A process for cleaning a material comprising the step of:
contacting a material with an extracting fluid under conditions of temperature and pressure sufficient to maintain the fluid at, near or above its critical point to produce a clean material.
2. The process of claim 1, wherein the extracting fluid is selected from the group consisting of comprising Xe, NH₃, lower aromatics, nitrous oxide, water, CO, CO₂, H₂O, lower alcohols, lower alkanes, lower alkenes and mixtures or combinations thereof.
3. The process of claim 1, wherein the extracting fluid comprises a major portion of CO₂ and a minor portion of a secondary fluid selected from the groups consisting of Xe, NH₃, lower aromatics, nitrous oxide, water, CO, H₂O, lower alcohols, lower alkanes, lower alkenes and mixtures or combinations thereof.
4. The process of claim 1, wherein the extracting fluid is CO₂
5. The process of claim 1, wherein the material is a drill fluid and the clean material comprises a hydrocarbon product substantially free of contaminants, a solids product substantially free of hydrocarbons and other contaminants, and an aqueous product.
6. The process of claim 1, wherein the material is a used oil and the clean material comprises a cleaned oil substantially free of water and water soluble contaminants.
7. The process of claim 6, wherein the cleaned oil has a lower sulfur content than the used oil.
8. The process of claim 1, wherein the material is a hydrocarbon fuel and the clean material comprises a cleaned fuel having a lower sulfur content than the hydrocarbon fuel prior to cleaning.

9. The process of claim 1, wherein the material is a hydrocarbon contaminated soil and the clean material comprises a hydrocarbon product substantially free of solids, water and water soluble contaminants, a cleaned soil substantially free of hydrocarbon and other contaminants, and an aqueous product substantially free of hydrocarbon.
10. A process for treating drilling fluids comprising the step of:
contacting a drill fluid with an extracting fluid under conditions of temperature and pressure sufficient to maintain the solvent at, near or above its critical point to produce a hydrocarbon product substantially free of contaminants, a solids product substantially free of hydrocarbons and other contaminants, and an aqueous product.
11. The process of claim 10, wherein the extracting fluid is selected from the group consisting of comprising Xe, NH₃, lower aromatics, nitrous oxide, water, CO, CO₂, H₂O, lower alcohols, lower alkanes, lower alkenes and mixtures or combinations thereof.
12. The process of claim 10, wherein the extracting fluid comprises a major portion of CO₂ and a minor portion of a secondary fluid selected from the groups consisting of Xe, NH₃, lower aromatics, nitrous oxide, water, CO, H₂O, lower alcohols, lower alkanes, lower alkenes and mixtures or combinations thereof.
13. The process of claim 10, wherein the extracting fluid is CO₂.
14. A cleaned drilling fluid solid comprising a solid material obtained from a process of any of the claim 10.
15. A hydrocarbon composition comprising a hydrocarbon material and drilling additives obtained from a process of any of the claim 10.
16. An aqueous composition comprising an aqueous material obtained from a process of any of the claim 10.

17. A process for treating used oil comprising the step of:
contacting a used oil with an extracting fluid under conditions of temperature and pressure sufficient to maintain the solvent at, near or above its critical point to produce a cleaned oil substantially free of water and water soluble contaminants.
18. The process of claim 17, wherein the extracting fluid is selected from the group consisting of comprising Xe, NH₃, lower aromatics, nitrous oxide, water, CO, CO₂, H₂O, lower alcohols, lower alkanes, lower alkenes and mixtures or combinations thereof.
19. The process of claim 17, wherein the extracting fluid comprises a major portion of CO₂ and a minor portion of a secondary fluid selected from the groups consisting of Xe, NH₃, lower aromatics, nitrous oxide, water, CO, H₂O, lower alcohols, lower alkanes, lower alkenes and mixtures or combinations thereof.
20. The process of claim 17, wherein the extracting fluid is CO₂
21. A process for treating hydrocarbon fuels drilling fluids comprising the step of:
contacting a hydrocarbon fuel with an extracting fluid under conditions of temperature and pressure sufficient to maintain the solvent at, near or above its critical point to produce a cleaned fuel having a lower sulfur content than the hydrocarbon fuel prior to cleaning.
22. The process of claim 21, wherein the extracting fluid is selected from the group consisting of comprising Xe, NH₃, lower aromatics, nitrous oxide, water, CO, CO₂, H₂O, lower alcohols, lower alkanes, lower alkenes and mixtures or combinations thereof.
23. The process of claim 21, wherein the extracting fluid comprises a major portion of CO₂ and a minor portion of a secondary fluid selected from the groups consisting of Xe, NH₃, lower aromatics, nitrous oxide, water, CO, H₂O, lower alcohols, lower alkanes, lower alkenes and mixtures or combinations thereof.
24. The process of claim 21, wherein the extracting fluid is CO₂

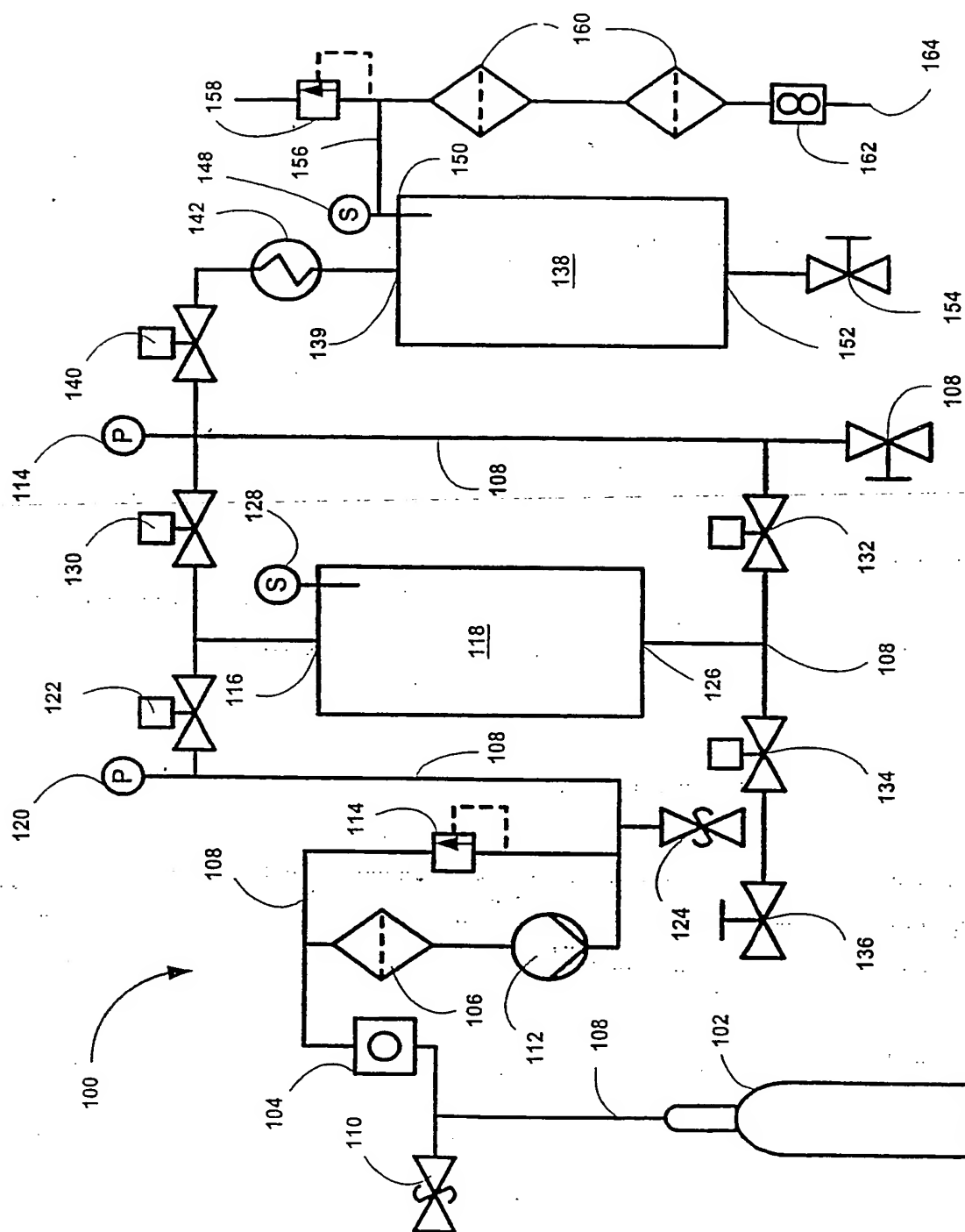


FIG. 1

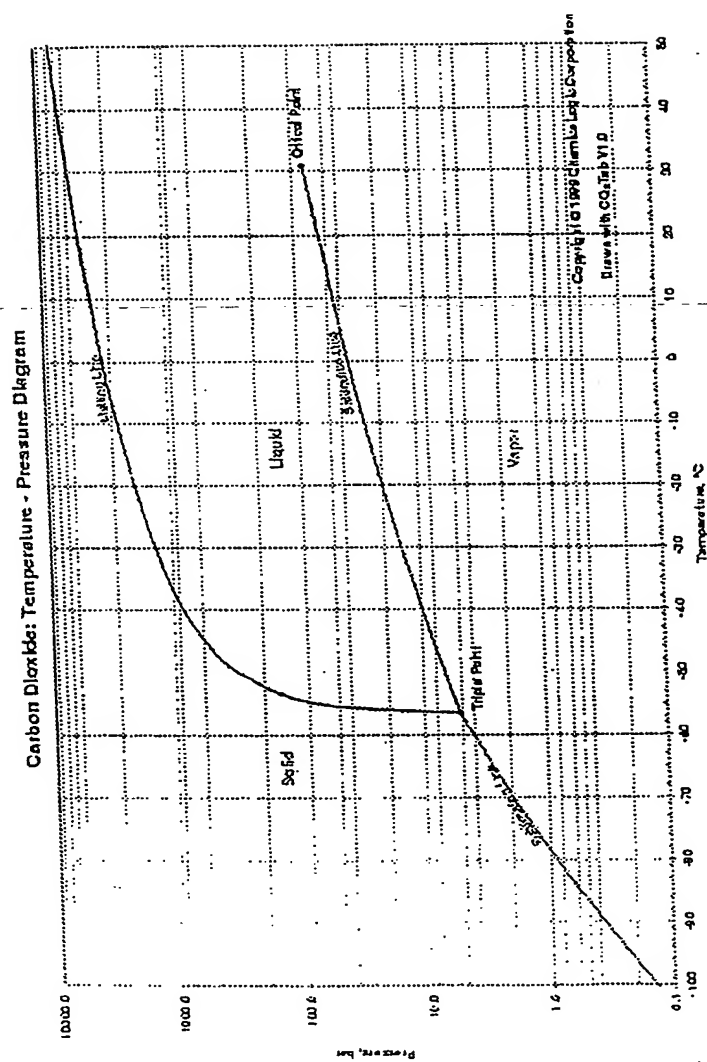
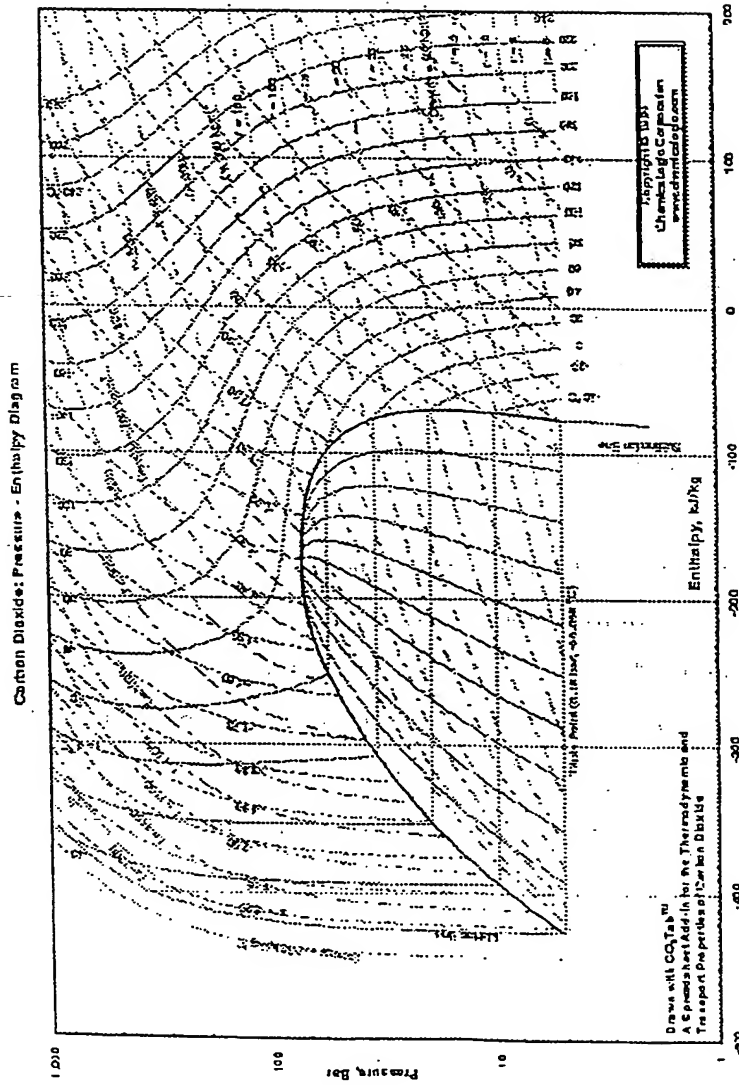


Fig. 2



List Of Useable Super Critical Fluids (fig.3)

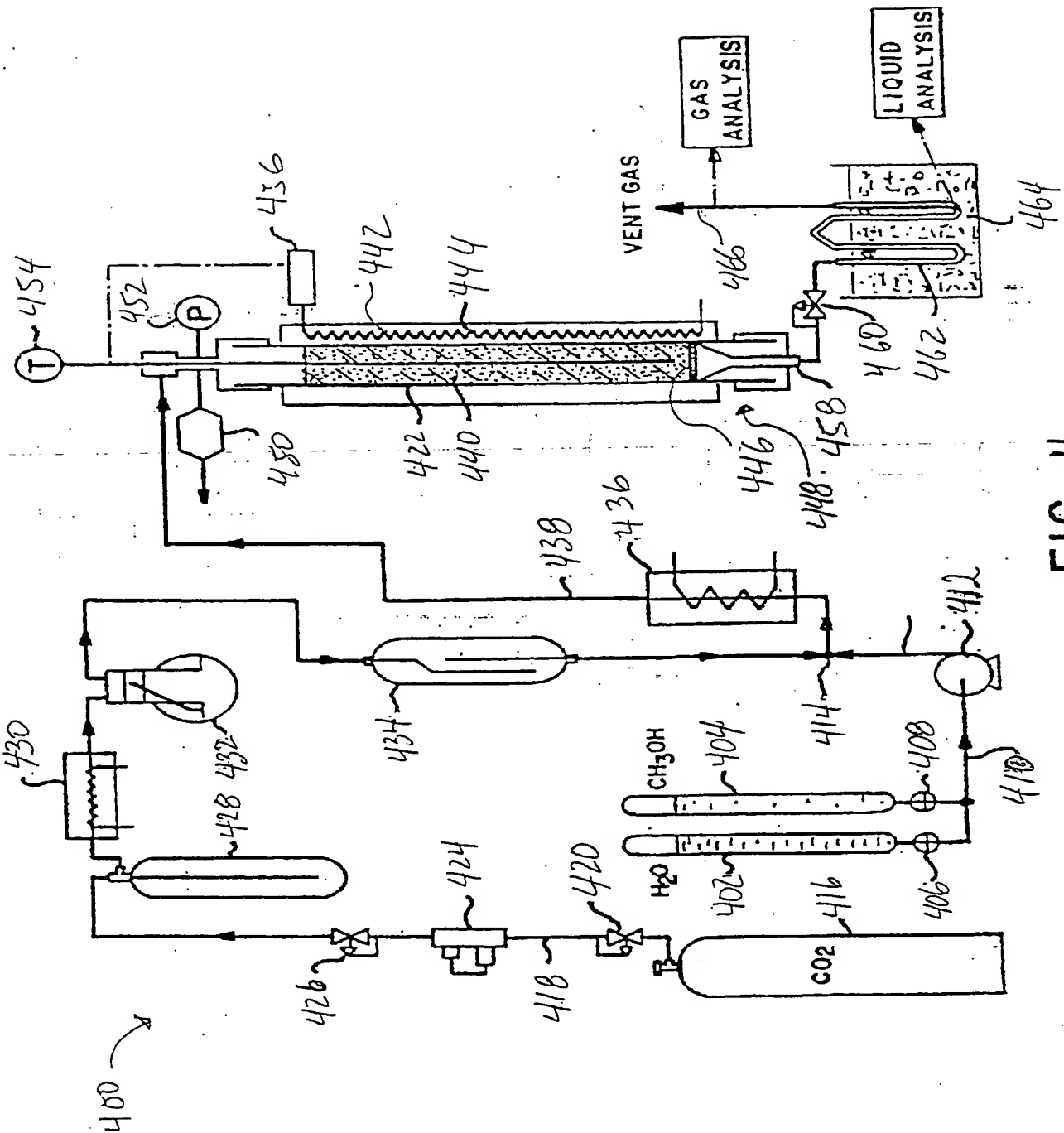
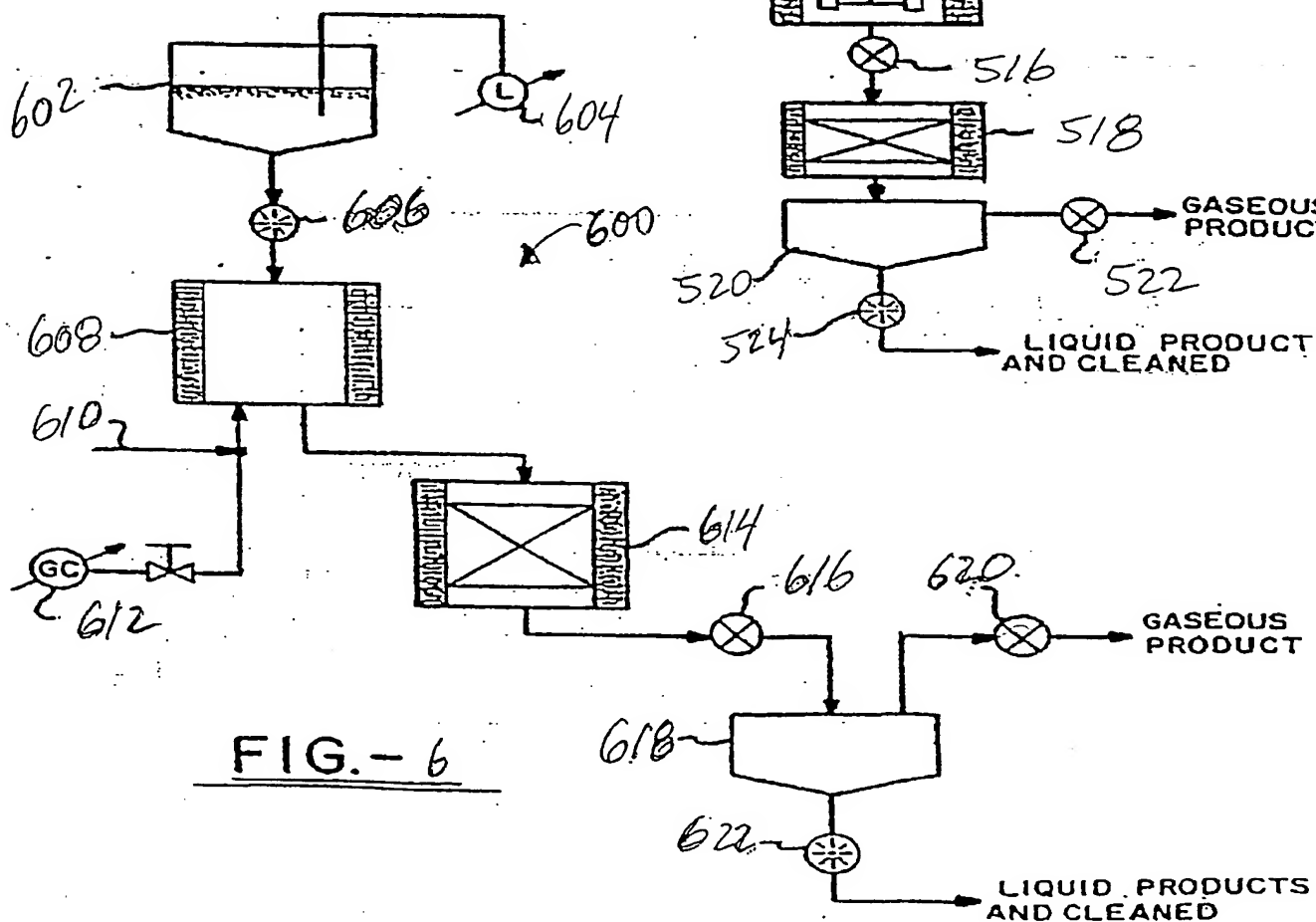
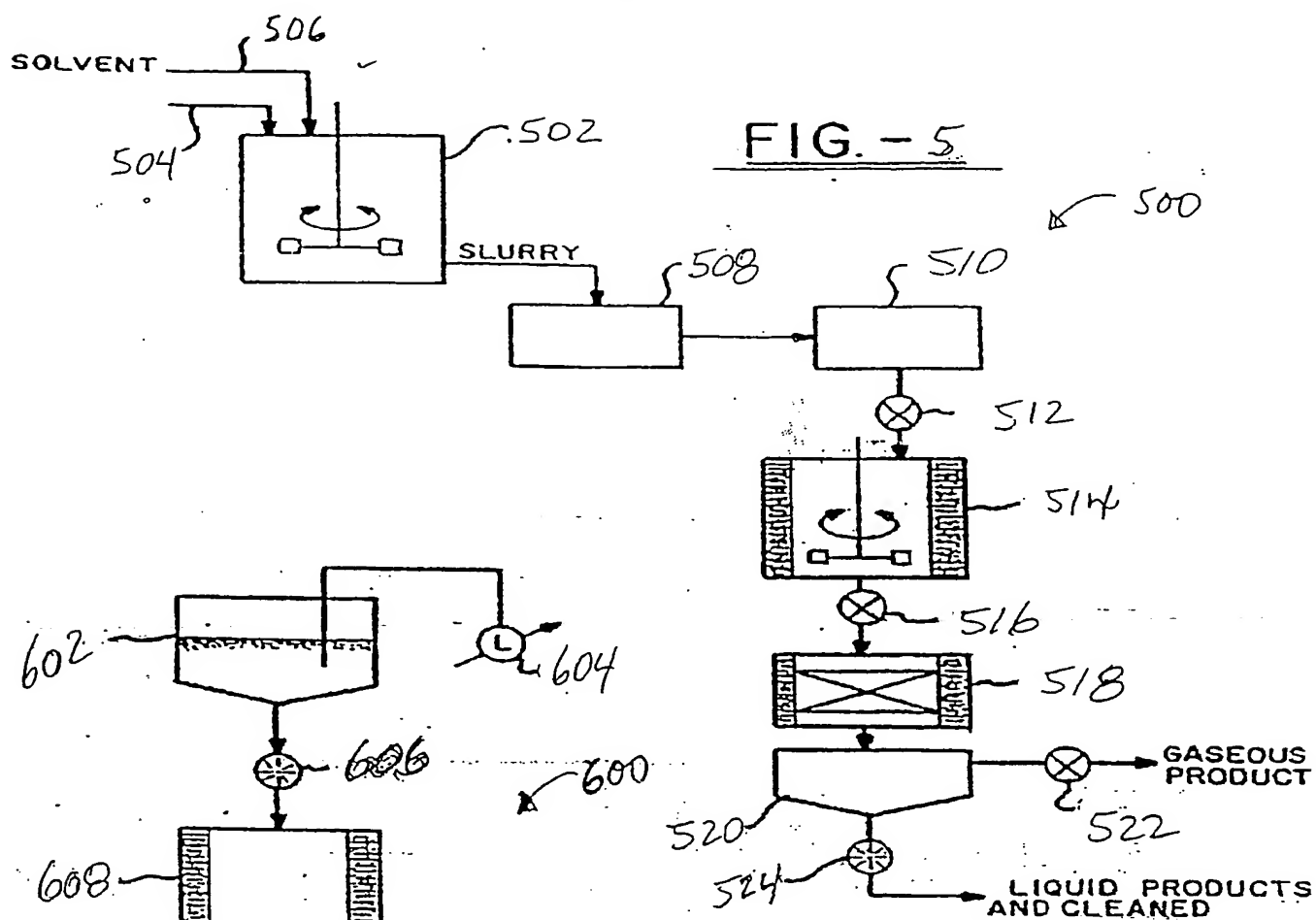


FIG. 4



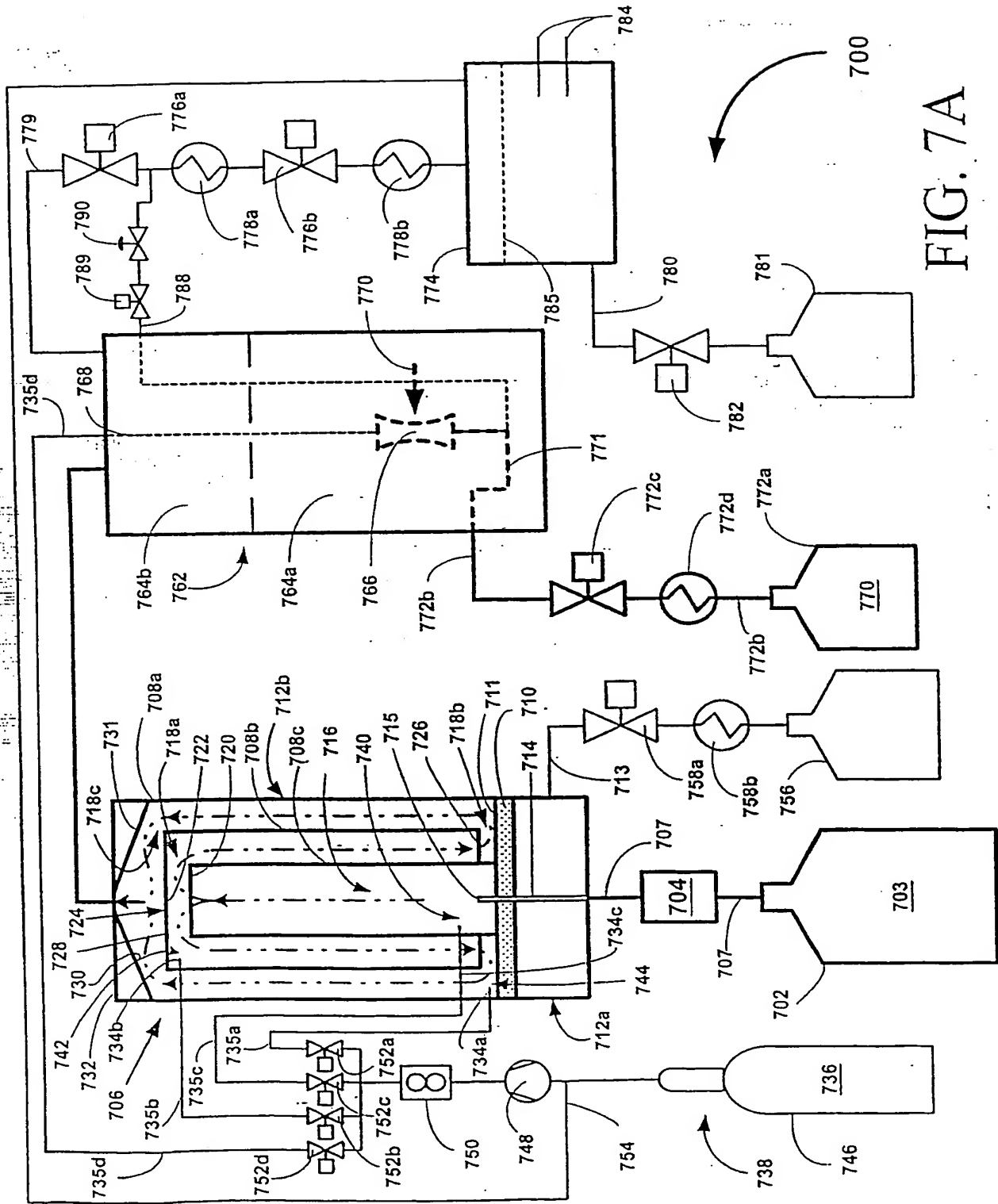


FIG. 7A

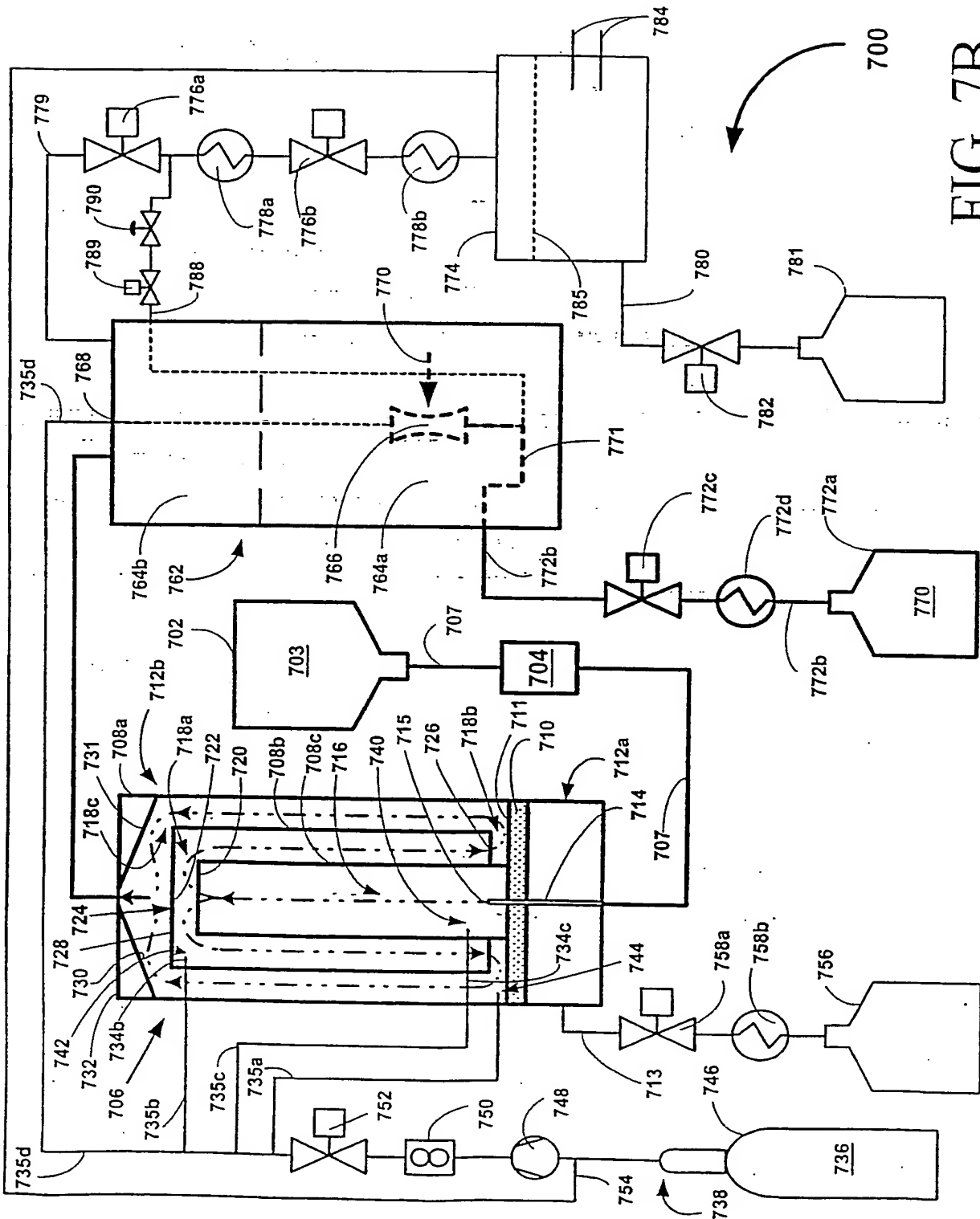


FIG. 7B

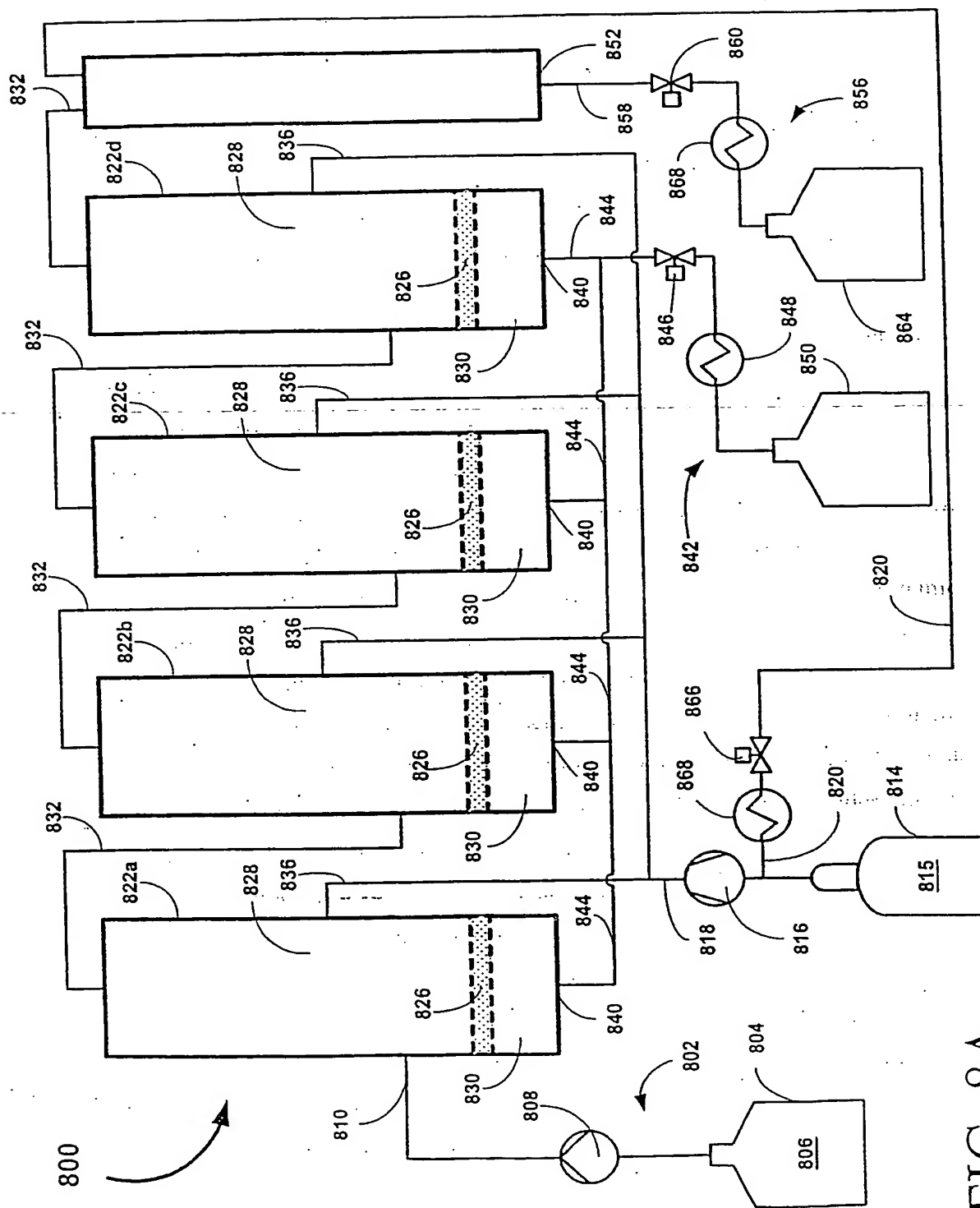


FIG. 8A

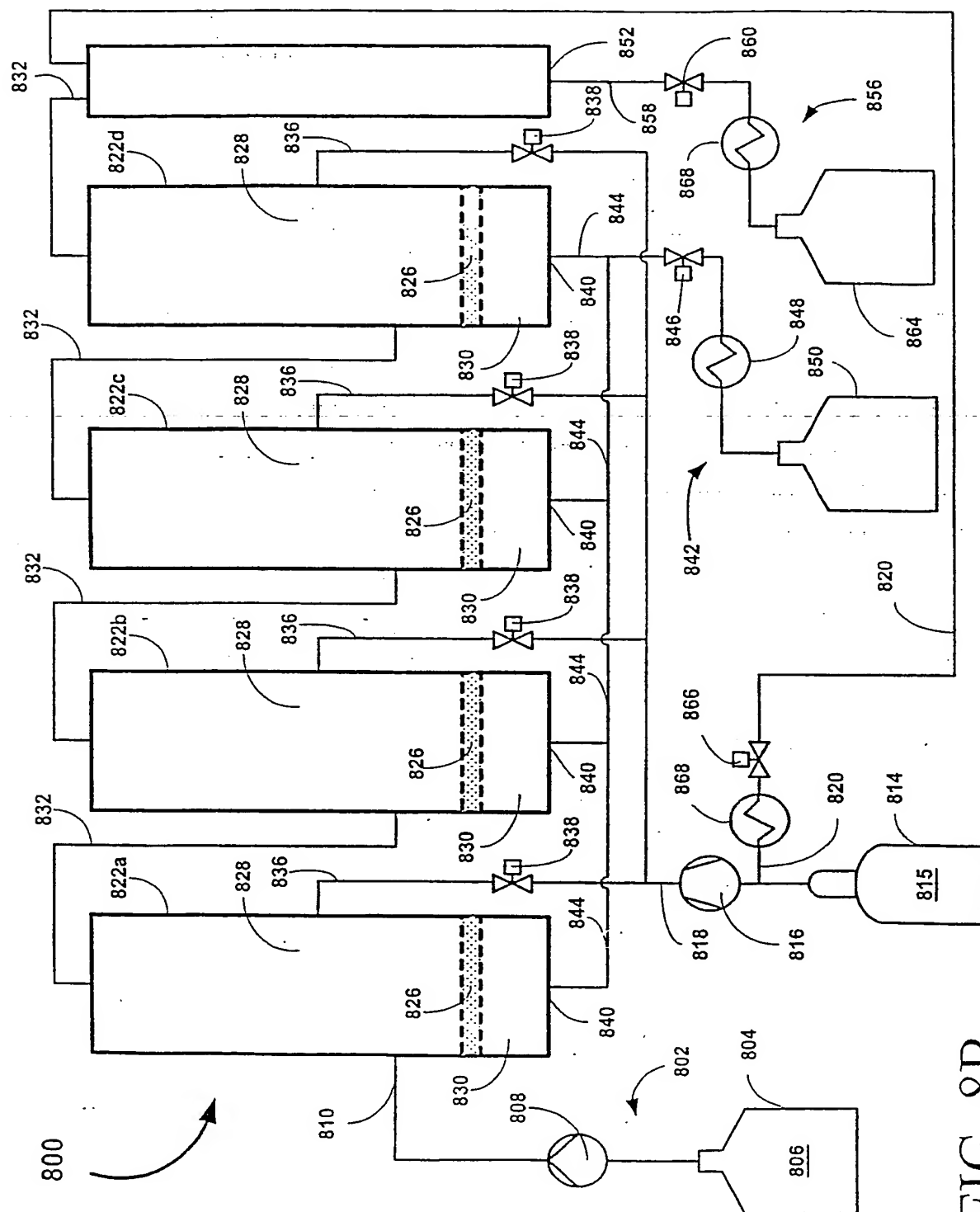


FIG. 8B

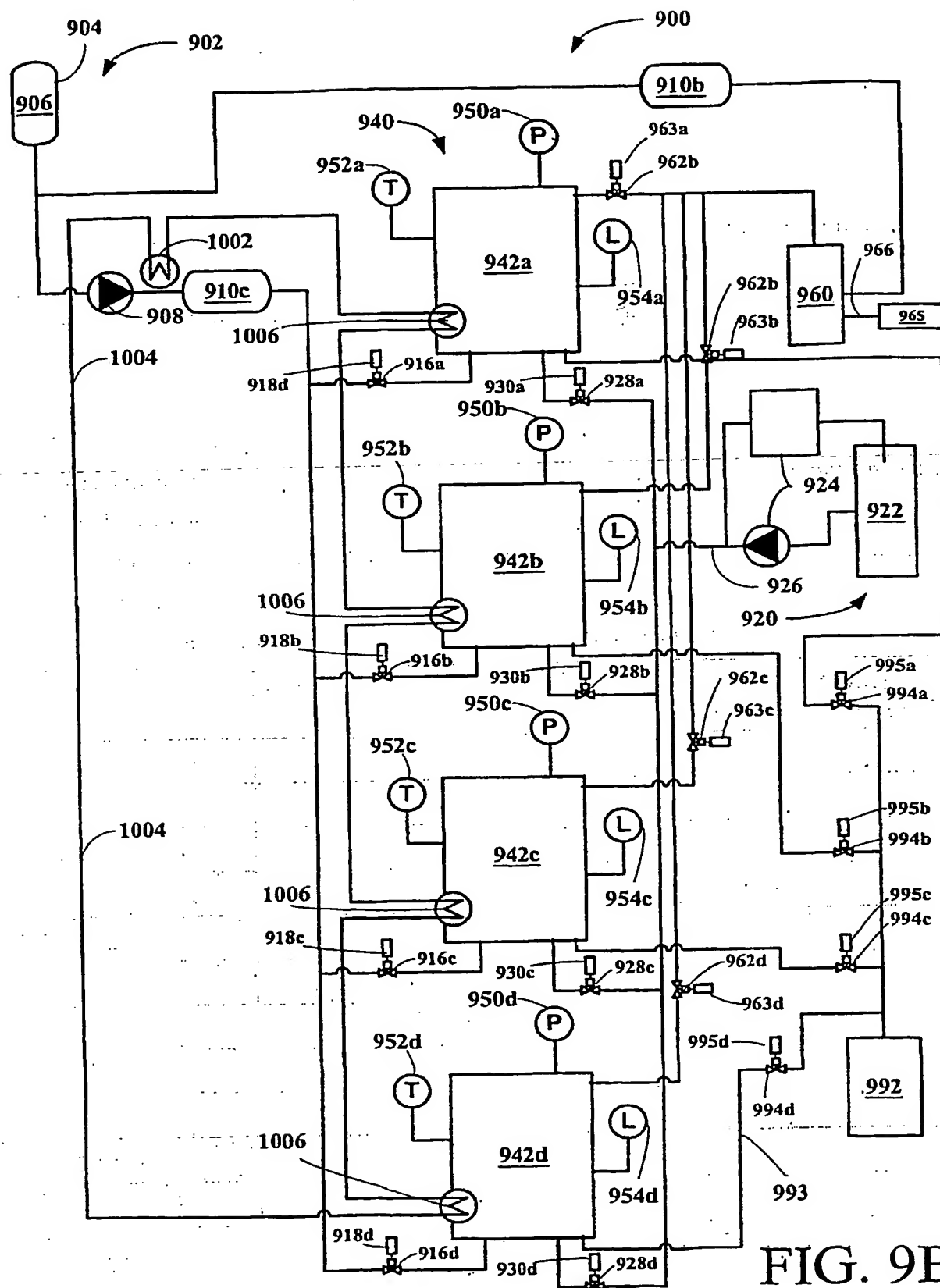


FIG. 9B

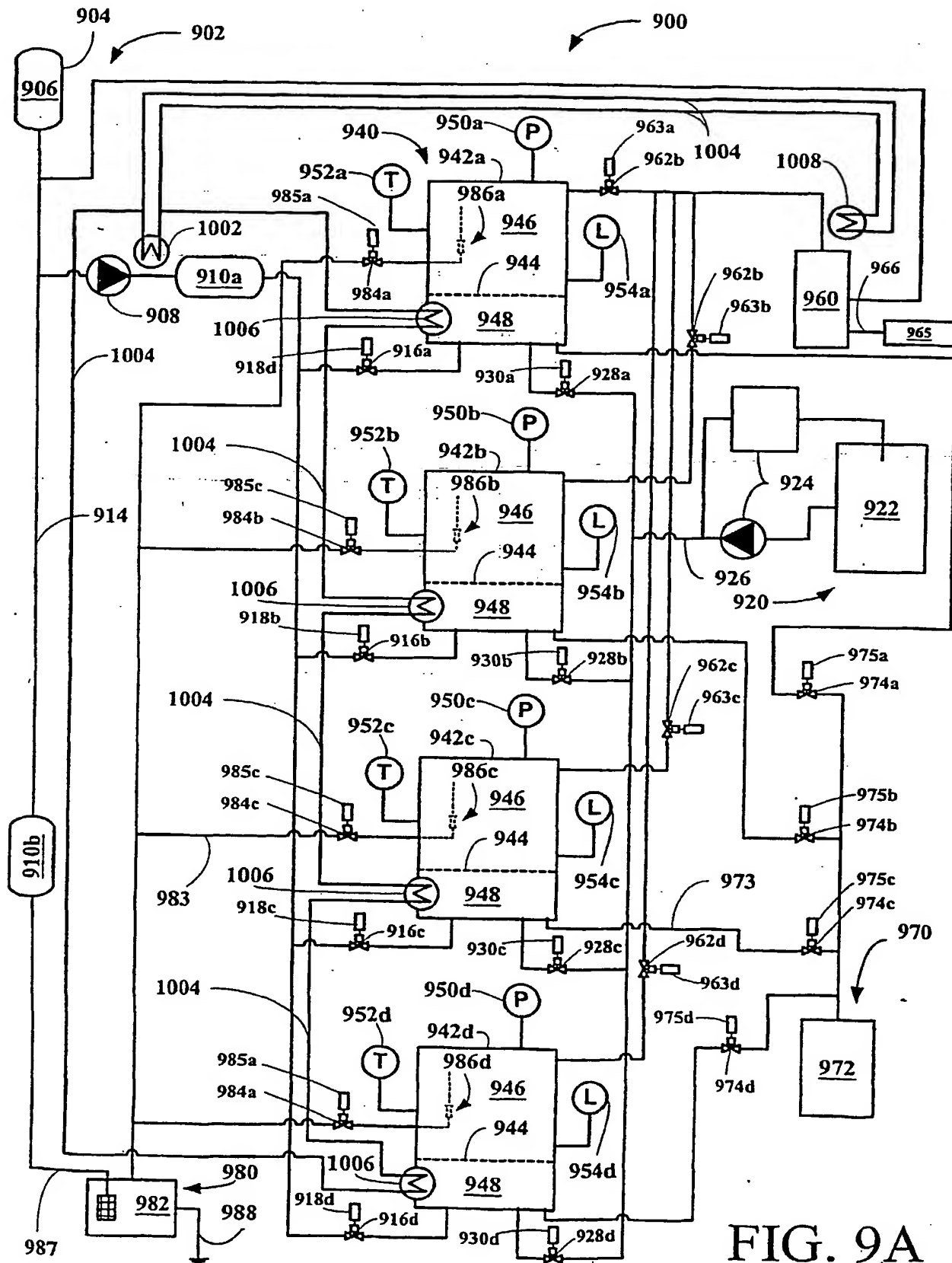


FIG. 9A

INTERNATIONAL SEARCH REPORT

International Application No

PCT/US 02/24207

A. CLASSIFICATION OF SUBJECT MATTER

IPC 7 B01D11/04 B01D11/02 C10G1/04 E21B21/06 A62D3/00
C10G1/00

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)

IPC 7 B01D C10G E21B A62D

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practical, search terms used)

EPO-Internal, WPI Data, PAJ

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X	US 4 824 570 A (BETHUEL LOUIS ET AL) 25 April 1989 (1989-04-25) column 1, line 6 - column 2, line 68 ---	1-4
X	US 4 341 619 A (POSKA FORREST L) 27 July 1982 (1982-07-27) column 1, line 42 - column 3, line 23 ---	1-4
X	US 1 805 751 A (BERTHOLD AUERBACH ERNST) 19 May 1931 (1931-05-19) claims -----	1-4

☐ Further documents are listed in the continuation of box C.☒ Patent family members are listed in annex.

* Special categories of cited documents:

- "A" document defining the general state of the art which is not considered to be of particular relevance
- "E" earlier document but published on or after the international filing date
- "L" document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)
- "O" document referring to an oral disclosure, use, exhibition or other means
- "P" document published prior to the international filing date but later than the priority date claimed

"T" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention

"X" document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone

"Y" document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art.

"&" document member of the same patent family

Date of the actual completion of the international search

25 October 2002

Date of mailing of the international search report

23. 01. 03

Name and mailing address of the ISA

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Authorized officer

Persichini, C

INTERNATIONAL SEARCH REPORT

Information on patent family members

International Application No.

PCT/US 02/24207

Patent document cited in search report		Publication date	Patent family member(s)	Publication date
US 4824570	A	25-04-1989	FR 2586938 A1	13-03-1987
			DE 3669440 D1	19-04-1990
			EP 0238527 A1	30-09-1987
			WO 8701299 A1	12-03-1987
US 4341619	A	27-07-1982	NONE	
US 1805751	A	19-05-1931	NONE	

INTERNATIONAL SEARCH REPORT

International application No.
PCT/US 02/24207

Box I Observations where certain claims were found unsearchable (Continuation of item 1 of first sheet)

This International Search Report has not been established in respect of certain claims under Article 17(2)(a) for the following reasons:

1. ☐ Claims Nos.:
because they relate to subject matter not required to be searched by this Authority, namely:

2. ☐ Claims Nos.:
because they relate to parts of the International Application that do not comply with the prescribed requirements to such an extent that no meaningful International Search can be carried out, specifically:

3. ☐ Claims Nos.:
because they are dependent claims and are not drafted in accordance with the second and third sentences of Rule 6.4(a).

Box II Observations where unity of invention is lacking (Continuation of item 2 of first sheet)

This International Searching Authority found multiple inventions in this international application, as follows:

see additional sheet

1. ☐ As all required additional search fees were timely paid by the applicant, this International Search Report covers all searchable claims.

2. ☐ As all searchable claims could be searched without effort justifying an additional fee, this Authority did not invite payment of any additional fee.

3. ☐ As only some of the required additional search fees were timely paid by the applicant, this International Search Report covers only those claims for which fees were paid, specifically claims Nos.:

4. ☒ No required additional search fees were timely paid by the applicant. Consequently, this International Search Report is restricted to the invention first mentioned in the claims; it is covered by claims Nos.:

1 to 4

Remark on Protest

- ☐ The additional search fees were accompanied by the applicant's protest.
- ☐ No protest accompanied the payment of additional search fees.

FURTHER INFORMATION CONTINUED FROM PCT/ISA/ 210

This International Searching Authority found multiple (groups of) inventions in this international application, as follows:

1. Claim: 1 to 4 -

Process for cleaning a material wherein specific extracting fluids at, near or above their critical points are utilized

2. Claims: 1, 5, 10 to 16

Process for cleaning drill fluid wherein the extracting fluid is at, near or above its critical point

3. Claims: 1, 6, 7, 17-20

Process for cleaning oil wherein the extracting fluid is at, near or above its critical point

4. Claims: 1, 8, 21 to 24

Process for cleaning fuel wherein the extracting fluid is at, near or above its critical point

5. Claims: 1, 9

Process for cleaning soil wherein the extracting fluid is at, near or above its critical point

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PN - JP4293890 A 19921019
 PD - 1992-10-19
 PR - JP19910059199 19910322
 OPD- 1991-03-22
 TI - TREATING METHOD AND DEVICE FOR SLURRY
 IN - TOZAWA FUMIAKI; ISHIZUKA KAORU; KUBO SOTOO; KURAMOTO KENJI; NAGASE SHINICHI
 PA - KAJIMA CORP; KURITA WATER IND LTD
 IC - C09K17/00 ; E02D5/18 ; E02D5/34 ; E21B21/06

© WPI / DERWENT

TI - Stabiliser liq. treatment - by mixing untreated stabiliser liq. with liq. contg. carbon dioxide gas dissolved under pressure
 PR - JP19910059199 19910322
 PN - JP4293890 A 19921019 DW199248 E21B21/06 006pp
 - JP7099075B B2 19951025 DW199547 E21B21/06 005pp
 PA - (KAJI) KAJIMA CORP
 - (KURK) KURITA WATER IND LTD
 IC - C09K17/00 ; E02D5/18 ; E02D5/34 ; E21B21/06
 AB - J04293890 Carbon dioxide gas is dissolved in part of a stabiliser liq. under pressure and then the liq. is mixed with an untreated stabiliser liq. under reduced pressure, to regenerate stabiliser liq.
 - Stabiliser liq. treatment appts. includes circulating bath to store stabiliser liq., stabiliser liq. supply passage to supply the liq. from the bath to the trench, stabiliser liq. circulating passage to circulate the liq. from the trench to the bath, carbon dioxide gas pressure-dissolving equipment to dissolve the gas in part of the liq. under pressure, and stabiliser liq. charging passage to charge the liq. from the pressure-dissolving appts. into the supply passage.
 - ADVANTAGE - Dissolves carbon dioxide into the entire stabiliser liq. efficiently(Dwg0/1)
 OPD- 1991-03-22
 AN - 1992-394590 [47]

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 IN - TOZAWA FUMIAKI; others:04
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 TI - TREATING METHOD AND DEVICE FOR SLURRY
 AB - PURPOSE: To improve the soluble efficiency of carbon dioxide gas to a stabilizing solution and the utilizing efficiency of the carbon dioxide gas by solving the carbon dioxide gas to a part of the stabilizer under applying a pressure, and then, mixing it to an untreated stabilizer under the pressure reducing condition so as to regenerate a stabilizer.

- CONSTITUTION: A stabilizing solution 3 is fed to a trench 2 from a circulation jar 1 through a stabilizer feeding passage 5, and the stabilizer 3 is recirculated to the circulation jar 1 through a stabilizer passage 7. In this case, a part of the stabilizer 3 is delivered to a carbon dioxide pressure-solving device 10 to pressure-solve the carbon dioxide gas, and then an untreated stabilizer 3 is mixed thereto under the pressure reducing condition to regenerate a stabilizer 3. By mixing the stabilizer 3 and the carbon dioxide gas under the pressure reducing condition in this case, the carbon dioxide gas of the larger amount than in the atmospheric pressure is solved in the stabilizer 3. And by making the stabilizer 3 in a pressure reducing condition, an oversaturated condition is generated, and the carbon dioxide gas exceeding the soluble degree is made into minute bubbles and separated. By mixing an untreated stabilizer 3 in such a condition, the gas-liquid contact efficiency is increased, and the carbon dioxide gas is solved in the untreated stabilizer efficiently.

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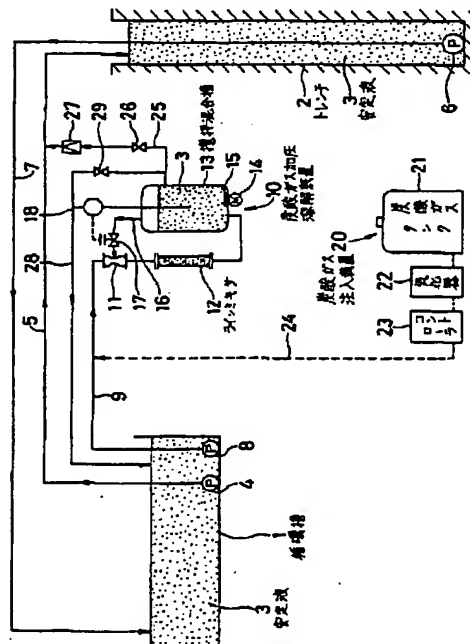
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(54) 【発明の名称】 安定液の処理方法および装置

(57) 【要約】

【目的】 泥水工法において使用される安定液への炭酸ガスの溶解効率が高く、一部の安定液に炭酸ガスを注入して他の安定液と混合することにより、全体の安定液に炭酸ガスを効率よく溶解して再生することができ、小型の装置と小動力で炭酸ガスを大量に溶解し、炭酸ガスの利用効率も高い安定液の処理方法および装置を提案する。

【構成】 循環槽からトレンチへ安定液を供給し、トレンチから安定液を循環槽へ循環させる系の安定液の処理方法であって、炭酸ガス加圧溶解装置において、安定液の一部に炭酸ガスを加圧下に溶解した後、減圧状態で未処理の安定液と混合して、減圧により発生する炭酸ガスの微細な気泡を未処理の安定液に溶解し、これにより安定液を再生するようにした安定液の処理方法および装置である。



【特許請求の範囲】

【請求項1】 泥水工法に用いられる安定液の処理方法において、安定液の一部に炭酸ガスを加圧下に溶解した後、減圧状態で未処理の安定液と混合して、安定液を再生することを特徴とする安定液の処理方法。

【請求項2】 安定液を貯留する循環槽と、循環槽からトレンチへ安定液を供給する安定液供給路と、トレンチから循環槽へ安定液を循環する安定液循環路と、安定液の一部に炭酸ガスを加圧溶解する炭酸ガス加圧溶解装置と、炭酸ガス加圧溶解装置から安定液を減圧して安定液供給路に注入する安定液注入路とを備えた安定液の処理装置。

【発明の詳細な説明】

【0001】

【産業上の利用分野】 本発明は泥水工法に用いられる安定液に炭酸ガスを溶解して再生する安定液の処理方法および装置に関するものである。

【0002】

【従来の技術】 地中（地下）連続壁工法、シールド工法、場所打ち杭工法などでは、トレンチの溝（孔）壁の安定化のために、安定液（泥水）を用いて掘削する泥水工法が採用されている。このような安定液としては、ベントナイトを主成分とする懸濁液が使用され、循環槽からトレンチに供給し、トレンチから循環槽に循環して使用されている。この安定液はセメント分から溶出するカルシウムイオンによってゲル化して粘度が上昇する性質がある。そこで安定液のゲル化等による劣化を防止する目的で、安定液に炭酸ガスを溶解して、カルシウムイオンを炭酸カルシウムとして析出させ、これにより安定液を再生して循環使用している。

【0003】 このような安定液の再生を行うための従来の処理方法としては、供給途中または循環槽内の安定液全量に対して炭酸ガスを注入して溶解する方法が行われている。具体的には例えば安定液の供給路にラインミキサまたは攪拌式の混合槽を配置して、炭酸ガスを注入した安定液を導いて炭酸ガスを溶解する方法、循環槽に炭酸ガスを吹込んで攪拌する方法、あるいはこれらを組合せた方法などがある。

【0004】 しかしながら、このような従来の安定液の処理方法においては、炭酸ガスの溶解効率が悪く、大量の炭酸ガスが必要であるにもかかわらず、炭酸ガスが無駄に排出されて、安定液中に大量の炭酸ガスを溶解させることができず、しかも安定液の全量を処理する必要があるため、装置が大型化し、消費動力が大きくなるなどの問題点があった。

【0005】

【発明が解決しようとする課題】 本発明の目的は、上記のような問題点を解決するため、安定液への炭酸ガスの溶解効率がよく、一部の安定液に炭酸ガスを注入して他の安定液と混合することにより、全体の安定液に炭酸ガ

スを効率よく溶解して再生することができ、小型の装置と小動力で炭酸ガスを大量に溶解し、炭酸ガスの利用効率も高い安定液の処理方法および装置を提案することである。

【0006】

【課題を解決するための手段】 本発明は次の安定液の処理方法および装置である。

【0007】 (1) 泥水工法に用いられる安定液の処理方法において、安定液の一部に炭酸ガスを加圧下に溶解した後、減圧状態で未処理の安定液と混合して、安定液を再生することを特徴とする安定液の処理方法。

【0008】 (2) 安定液を貯留する循環槽と、循環槽からトレンチへ安定液を供給する安定液供給路と、トレンチから循環槽へ安定液を循環する安定液循環路と、安定液の一部に炭酸ガスを加圧溶解する炭酸ガス加圧溶解装置と、炭酸ガス加圧溶解装置から安定液を減圧して安定液供給路に注入する安定液注入路とを備えた安定液の処理装置。

【0009】 本発明の安定液の処理方法において、炭酸ガスを加圧溶解する安定液は循環槽、安定液供給路、安定液循環路のいずれの安定液でもよい。安定液に炭酸ガスを溶解するときの圧力は特に限定されず、圧力が高いほど大量の炭酸ガスが溶解するが、 1 kg f/cm^2 以上が好ましく、特に $1\sim 5\text{ kg f/cm}^2$ 、好ましくは $2\sim 3\text{ kg f/cm}^2$ の圧力にすると、汎用の装置が使用できる。

【0010】 炭酸ガスを加圧溶解した後の安定液と混合する未処理の安定液としては、安定液供給路の安定液が好ましいが、循環槽または安定液循環路の安定液でもよい。炭酸ガスを加圧溶解後、未処理の安定液と混合するときの減圧は、上記加圧状態を解除する程度でよく、安定液をトレンチに供給するための圧力は加えておくことができる。

【0011】 炭酸ガス加圧溶解装置としては、ラインミキサと攪拌混合槽の組合せが好ましいが、他の類似の手段でもよい。攪拌混合槽で未溶解のまま分離する炭酸ガスは、ラインミキサの前の安定液に注入して溶解することができる。

【0012】 炭酸ガスを加圧溶解する安定液の量は圧力によって異なるが、 $2\sim 3\text{ kg f/cm}^2$ の圧力の場合は全体の $1/2$ ないし $1/3$ 程度でよい。炭酸ガスの加圧溶解に要する時間は、通常ラインミキサでは1秒間以内、攪拌混合槽では1～3分間程度である。

【0013】

【作用】 本発明の安定液の処理装置においては、循環槽から安定液供給路を通してトレンチへ安定液を供給し、トレンチから安定液循環路を通して循環槽へ安定液を循環する。このとき安定液の一部を炭酸ガス加圧溶解装置に送液して炭酸ガスを加圧溶解した後、減圧状態で未処理の安定液を混合して、安定液を再生する。

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【0014】安定液と炭酸ガスを加圧下に混合すると、大気圧下におけるよりも大量の炭酸ガスが安定液中に溶解する。この安定液を減圧状態にすると、過飽和状態となり、溶解度を超える炭酸ガスが微細な気泡となって分離する。この状態で未処理の安定液を混合すると、分離した炭酸ガスが微細な気泡の状態でも未処理の安定液と接触するため、気液接触効率が高く、炭酸ガスは効率よく未処理の安定液中に溶解し、安定液は再生される。

【0015】このため炭酸ガスの溶解効率は高く、炭酸ガスが有効に利用されて、無駄に排出されることはなく、また炭酸ガスは安定液中に大量に溶解する。そして炭酸ガスを加圧溶解する安定液は一部でよいから、小型の装置および小動力で炭酸ガスは効率よく溶解する。

【0016】炭酸ガス加圧溶解装置としてラインミキサおよび攪拌混合槽を用いる場合は、炭酸ガスを注入した安定液はラインミキサを通過するときに、気液が細分化された状態で接触し、この状態で攪拌混合槽で加圧下に混合されるため、炭酸ガスの溶解速度が大きくなる。

【0017】このとき攪拌混合槽で未溶解のまま分離する炭酸ガスを、ラインミキサの前の安定液に注入することにより、炭酸ガスの利用率はさらに高くなり、無駄に排棄される炭酸ガスの量は少なくなる。

【0018】

【実施例】以下、本発明を図面の実施例により説明する。図1は実施例の安定液の処理方法および装置を示す系統図である。

【0019】図において、1は循環槽、2はトレンチである。循環槽1から安定液3をポンプ4によりトレンチ2に供給するように安定液供給路5が設けられ、トレンチ2から安定液3をポンプ6により循環槽1へ循環するように安定液循環路7が設けられている。

【0020】10は炭酸ガス加圧溶解装置であり、循環槽1から安定液3の一部をポンプ8により送液する安定液送液路9に設けられたエジェクタ11、ラインミキサ12および攪拌混合槽13からなる。攪拌混合槽13の底部にはモータ14により回転する攪拌機15が設けられている。攪拌混合槽13の頂部から炭酸ガス返送管16が弁17を介してエジェクタ11に連絡している。攪拌混合槽13の上部にはレベルスイッチ18が設けられており、攪拌混合槽13内の安定液3の液面が下がったときに弁17を開くように接続している。

【0021】20は炭酸ガス注入装置であり、炭酸ガスタンク21、気化器22およびコントローラ23を有する炭酸ガス注入路24が安定液送液路9に接続している。25は安定液注入路であり、炭酸ガス加圧溶解装置10から弁26、減圧ノズル27を介して安定液供給路5に接続している。28は安定液返送路であり、炭酸ガス加圧溶解装置10から弁29を介して循環槽1に接続している。

【0022】上記の安定液処理装置においては、循環槽

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1からポンプ4により安定液供給路5を通してトレンチ2へ安定液3を供給し、トレンチ2からポンプ6により安定液循環路7を通して循環槽1へ安定液3を循環する。そして循環槽1の安定液3の一部を、ポンプ8により安定液送液路9から炭酸ガス加圧溶解装置10に送液して炭酸ガスを加圧溶解し、安定液を再生する。

【0023】このとき炭酸ガス注入装置20の炭酸ガスタンク21の液化炭酸ガスを気化器22で気化し、コントローラ23で流量を調整して、炭酸ガス注入路24から安定液送液路9中の安定液に炭酸ガスを加圧状態で注入する。

【0024】炭酸ガス加圧溶解装置10では、炭酸ガスを注入した安定液がエジェクタ11を通過する際、攪拌混合槽13の頂部から未溶解の炭酸ガスを吸入する。そして炭酸ガスを注入した安定液はラインミキサ12を通過するときに、気液が細分化され、この状態で攪拌混合槽13に入り、攪拌機15により加圧下に混合され、これにより炭酸ガスの溶解速度が大きくなり、大量の炭酸ガスが安定液に溶解し、安定液が再生される。

【0025】攪拌混合槽13において炭酸ガスを加圧溶解した安定液は、安定液注入路25から弁26を経て、減圧ノズル27で減圧し、安定液供給路5の未処理の安定液と混合して、未処理の安定液を再生し、トレンチ2に供給される。

【0026】炭酸ガス加圧溶解装置10において、安定液と炭酸ガスを加圧下に混合すると、大気圧下におけるよりも大量の炭酸ガスが安定液中に溶解する。この安定液を減圧状態にすると、過飽和状態となり、溶解度を超える炭酸ガスが微細な気泡となって分離する。この状態で未処理の安定液を混合すると、分離した炭酸ガスが微細な気泡の状態でも未処理の安定液と接触するため、気液接触効率が高く、炭酸ガスは効率よく未処理の安定液中に溶解し、安定液は再生される。

【0027】攪拌混合槽13ではレベルスイッチ18により安定液の液面を検出し、未溶解の炭酸ガスがたまって液面が下がったとき弁17を開いて、未溶解の炭酸ガスをエジェクタ11により安定液に吸入する。このようにして攪拌混合槽13で未溶解のまま分離する炭酸ガスをラインミキサ12の前の安定液に注入することにより、炭酸ガスの利用率は高くなり、無駄に排棄される炭酸ガスの量は少なくなる。

【0028】循環槽1内の安定液3の劣化が激しいときは、炭酸ガス加圧溶解装置10で炭酸ガスを加圧溶解して再生した安定液を安定液返送路28から循環槽1に返送し、循環槽1内の安定液3を再生する。

【0029】上記の安定液の処理方法では、炭酸ガスの溶解効率は高く、炭酸ガスが有効に利用されて、無駄に排棄されることはなく、また炭酸ガスは安定液中に大量に溶解する。そして炭酸ガスを加圧溶解する安定液は一部でよいから、小型の装置および小動力で炭酸ガスは効

率よく溶解する。

【0030】このような安定液の処理方法によると、従来法で再生できなかった600~700m³/hr程度の大量の安定液でも、小型の装置により大量の炭酸ガスを溶解して、効率よく再生することができる。

【0031】なお、上記実施例では、循環槽1の安定液3の一部を炭酸ガス加圧溶解装置10に送液したが、安定液供給路5または安定液循環路7の安定液の一部を炭酸ガス加圧溶解装置10に送液してもよい。

【0032】

【発明の効果】本発明によれば、安定液の一部に炭酸ガスを加圧下に溶解した後、減圧状態で未処理の安定液と混合して安定液を再生するようにしたので、安定液への炭酸ガスの溶解効率が高く、一部の安定液に炭酸ガスを注入して他の安定液と混合することにより、全体の安定液に炭酸ガスを効率よく溶解して再生することができ、小型の装置と小動力で炭酸ガスを大量に溶解し、炭酸ガスの利用効率も高い安定液の処理方法および装置が得られる。

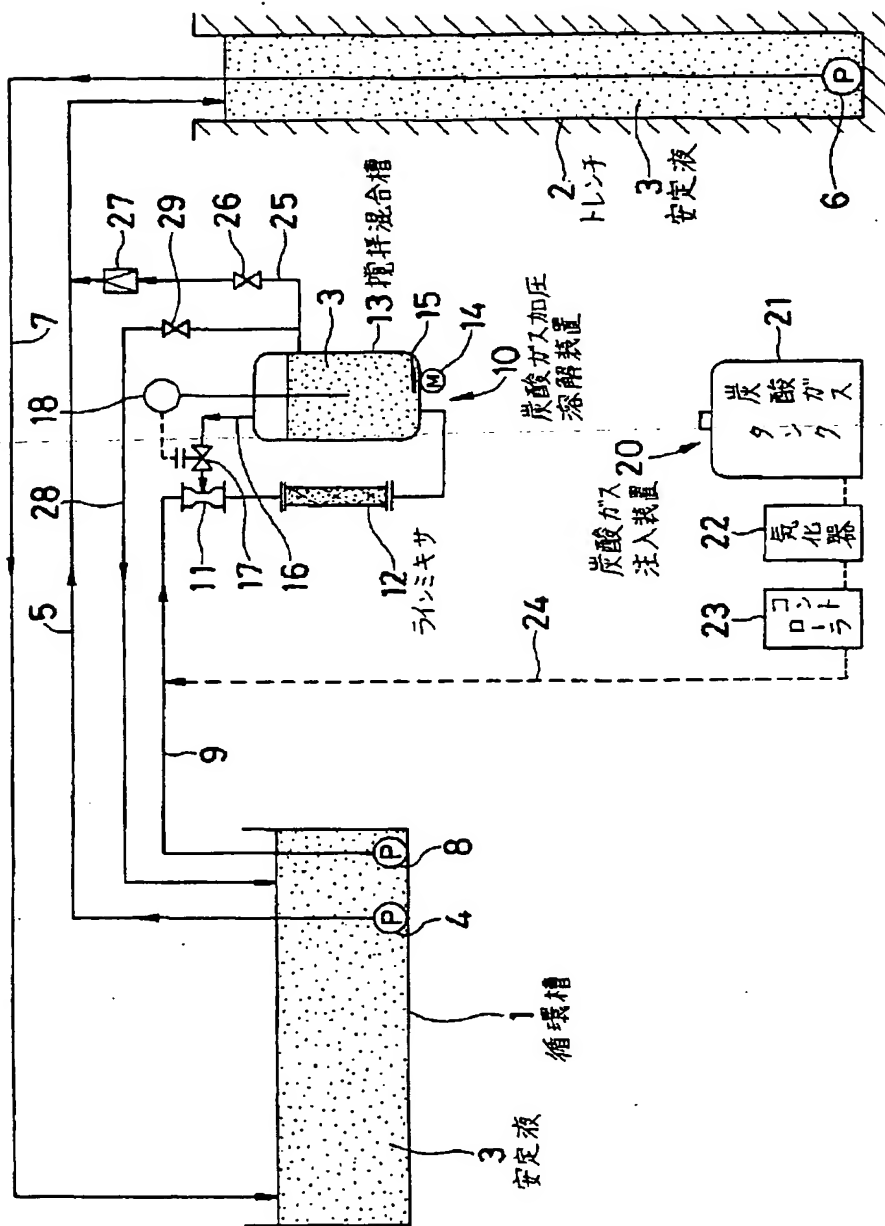
【図面の簡単な説明】

【図1】実施例の安定液の処理方法および装置を示す系統図である。

【符号の説明】

- 1 循環槽
- 2 トレンチ
- 3 安定液
- 4、6、8 ポンプ
- 5 安定液供給路
- 7 安定液循環路
- 9 安定液送液路
- 10 炭酸ガス加圧溶解装置
- 11 エジェクタ
- 12 ラインミキサ
- 13 攪拌混合槽
- 14 モータ
- 15 攪拌機
- 17、26、29 弁
- 18 レベルスイッチ
- 20 炭酸ガス注入装置
- 21 炭酸ガスタンク
- 22 気化器
- 23 コントローラ
- 24 炭酸ガス注入路
- 25 安定液注入路
- 27 減圧ノズル
- 28 安定液返送路

【図1】



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